Banner appropriate to article type will appear here in typeset article

# Flow of an Oldroyd-B fluid in a slowly varying contraction: theoretical results for arbitrary values of Deborah number in the ultra-dilute limit

# 4 Evgeniy Boyko<sup>1</sup><sup>†</sup>, John Hinch<sup>2</sup> and Howard A. Stone<sup>3</sup>

5 <sup>1</sup>Faculty of Mechanical Engineering, Technion – Israel Institute of Technology, Haifa 3200003, Israel

- 6 <sup>2</sup>DAMTP-CMS, Cambridge University, Wilberforce Road, Cambridge CB3 0WA, UK
- 7 <sup>3</sup>Department of Mechanical and Aerospace Engineering, Princeton University, Princeton, NJ 08544, USA

8 (Received xx; revised xx; accepted xx)

Pressure-driven flows of viscoelastic fluids in narrow non-uniform geometries are common 9 in physiological flows and various industrial applications. For such flows, one of the main 10 interests is understanding the relationship between the flow rate q and the pressure drop  $\Delta p$ , 11 which, to date, is studied primarily using numerical simulations. We analyze the flow of 12 the Oldroyd-B fluid in slowly varying arbitrarily shaped, contracting channels and present a 13 theoretical framework for calculating the  $q - \Delta p$  relation. We apply lubrication theory and 14 consider the ultra-dilute limit, in which the velocity profile remains parabolic and Newtonian, 15 resulting in a one-way coupling between the velocity and polymer conformation tensor. 16 This one-way coupling enables us to derive closed-form expressions for the conformation 17 tensor and the flow rate-pressure drop relation for arbitrary values of the Deborah number 18 (De). Furthermore, we provide analytical expressions for the conformation tensor and the 19  $q - \Delta p$  relation in the high Deborah limit, complementing our previous low-Deborah-number 20 lubrication analysis. We reveal that the pressure drop in the contraction monotonically 21 decreases with *De*, having linear scaling at high Deborah numbers, and identify the physical 22 mechanisms governing the pressure drop reduction. We further elucidate the spatial relaxation 23 of elastic stresses and pressure gradient in the exit channel following the contraction and show 24 that the downstream distance required for such relaxation scales linearly with De. 25

# 26 1. Introduction

Viscoelastic fluid flows in non-uniform geometries consisting of contractions or expansions 27 occur in physiological flows, e.g., arterial flows that may have such shape changes due to 28 thrombus formation (Westein et al. 2013), and in various industrial applications (Pearson 29 1985). For such flows, one of the key interests is to understand the dependence of the pressure 30 drop  $\Delta p$  on the flow rate q. It is well known that adding even small amounts of polymer 31 molecules in a Newtonian solvent may drastically change the hydrodynamic features of the 32 flow of the solution due to polymer stretching, which generates elastic stresses in addition to 33 viscous stresses (Bird et al. 1987; Steinberg 2021; Alves et al. 2021; Datta et al. 2022). 34

35 Pressure-driven flows of viscoelastic fluids and the corresponding flow rate-pressure drop

† Email address for correspondence: evgboyko@technion.ac.il

# Abstract must not spill onto p.2

36 relation have been studied extensively in various geometries, mainly through numerical

<sup>37</sup> simulations (Szabo *et al.* 1997; Alves *et al.* 2003; Binding *et al.* 2006; Alves & Poole 2007;

Zografos *et al.* 2020; Varchanis *et al.* 2022) and experimental measurements (Rothstein &
McKinley 1999, 2001; Sousa *et al.* 2009; Ober *et al.* 2013; James & Roos 2021). We refer

40 the reader to overviews given recently by Boyko & Stone (2022) and Hinch *et al.* (2023).

In particular, the abrupt contraction and contraction-expansion channels have received 41 42 much attention (Rothstein & McKinley 1999; Alves et al. 2003; Binding et al. 2006; Ferrás et al. 2020), and 4:1 two-dimensional (2-D) and axisymmetric contraction flows have 43 become benchmark flow problems in computational non-Newtonian fluid mechanics (Alves 44 et al. 2021). Numerical simulations of viscoelastic fluid flow in these and other non-uniform 45 geometries include a long downstream (exit) section to allow the stresses to reach their 46 47 fully relaxed values (see, e.g., Debbaut et al. 1988; Alves et al. 2003). This is because once perturbed from their fully relaxed values, the elastic stresses require a long distance for spatial 48 relaxation to enable stable and converged numerical solutions. For higher Deborah (De) or 49

50 Weissenberg (Wi) numbers (see definitions in § 2.1), a longer downstream section is required 51 (Keiller 1993).

Therefore, understanding the spatial relaxation of elastic stresses, velocity, and pressure is of both fundamental and practical importance, as that determines the size of the computational domain (Alves *et al.* 2003). However, despite extensive study of viscoelastic channel flows,

55 the spatial relaxation of stresses and pressure in these geometries is not well understood. As 56 a result, the length of the exit channel is currently set somewhat arbitrarily, thus motivating

57 the development of theory. Furthermore, in many applications, it is necessary to determine

58 the *total* pressure drop over the configuration for a given flow rate, thus requiring to account

59 for the pressure drop in the entry and exit channels. However, most studies to date focused

on the non-uniform region or close vicinity of the abrupt contraction and reported a suitably

61 non-dimensionalized so-called Couette correction (or excess pressure drop), rather than the

62 total non-dimensional pressure drop in the entire configuration (see, e.g., Alves *et al.* 2003;

63 Rothstein & McKinley 1999; Binding *et al.* 2006), presumably due to the arbitrariness of the 64 exit channel length in simulations.

One widely used approach to obtain theoretical results in different viscoelastic fluid flow 65 problems relies on considering the weakly viscoelastic limit by applying a perturbation 66 expansion in powers of the Deborah or Weissenberg number, which are assumed to be 67 68 small (see, e.g., Datt et al. 2017, 2018; Datt & Elfring 2019; Gkormpatsis et al. 2020; Housiadas et al. 2021; Dandekar & Ardekani 2021; Su et al. 2022). In particular, there 69 have been many applications of such an expansion in conjunction with lubrication theory in 70 studying thin films and tribology problems (Ro & Homsy 1995; Tichy 1996; Sawyer & Tichy 71 1998; Zhang et al. 2002; Saprykin et al. 2007; Ahmed & Biancofiore 2021; Gamaniel et al. 72 73 2021; Ahmed & Biancofiore 2023). Recently, we have applied lubrication theory and such an expansion in powers of *De*, developing a reduced-order model for the steady flow of an 74 Oldroyd-B fluid in a slowly varying, arbitrarily-shaped 2-D channel (Boyko & Stone 2022). 75 In particular, we provided analytical expressions for the velocity and stress fields and the flow 76 rate-pressure drop relation in the non-uniform region up to  $O(De^2)$ . We further exploited 77 the reciprocal theorem (Boyko & Stone 2021, 2022) to obtain the flow rate-pressure drop 78 79 relation at the next order,  $O(De^3)$ .

However, the low-Deborah-number analysis cannot accurately capture the behavior at high *De* numbers where there are significant elastic stresses. Another approach to simplifying the governing equations while capturing the underlying physics at non-small Deborah numbers is to consider the ultra-dilute limit (Remmelgas *et al.* 1999; Moore & Shelley 2012; Li *et al.* 2019; Mokhtari *et al.* 2022),  $\tilde{\beta} = \mu_p/\mu_0 \ll 1$ , where  $\mu_p$  is the polymer contribution to the total zero-shear-rate viscosity  $\mu_0$  of the polymer solution. Physically, the ultra-dilute limit

corresponds to a low concentration of polymer molecules in a Newtonian solvent, such that 86 the viscosity of the polymer solution,  $\mu_0$ , is only slightly larger than the solvent viscosity, 87  $\mu_s$  (Remmelgas *et al.* 1999; Mokhtari *et al.* 2022). Furthermore, the limit  $\tilde{\beta} = \mu_p/\mu_0 \ll 1$ 88 is closely related to the diluteness criterion of a constant shear-viscosity viscoelastic Boger 89 90 fluid (Moore & Shelley 2012). In the ultra-dilute limit, the flow field approximated as Newtonian creates elastic stresses that are not coupled back to change the flow. These elastic 91 92 stresses can then be used to find the correction to the velocity and pressure fields due to fluid viscoelasticity, even at high Deborah numbers. Previous studies used this approach to 93 determine the structure of the stress distribution in the flow around a cylinder (Renardy 2000). 94 a sphere (Moore & Shelley 2012), and arrays of cylinders (Mokhtari et al. 2022), as well as 95 in the stagnation (Becherer et al. 2009; Van Gorder et al. 2009) and cross-slot (Remmelgas 96 97 et al. 1999) flows.

In this work, we continue our theoretical studies (Boyko & Stone 2022; Hinch et al. 2023) of 98 the pressure-driven flow of the Oldroyd-B fluid in slowly varying, arbitrarily shaped, narrow 99 channels. In contrast to Boyko & Stone (2022), who focused only on the flow through a 100 101 non-uniform channel in the low-Deborah-number limit, and Hinch et al. (2023), who studied numerically the flow through a contraction, expansion, and constriction for order-one Deborah 102 numbers, and also provided asymptotic description at high Deborah numbers, current work 103 examines the ultra-dilute limit and arbitrary values of Deborah number. Specifically, we 104 analyze the flow of the Oldroyd-B fluid in a contracting geometry and the relaxation of the 105 106 elastic stresses and pressure in the exit channel. We apply the lubrication approximation 107 and use a one-way coupling between the velocity and polymer stresses to derive semi-108 analytical expressions for the conformation tensor in the contraction and the exit channel for arbitrary values of the Deborah number in the ultra-dilute limit. These semi-analytical 109 110 expressions allow us to calculate the pressure drop and elucidate the relaxation of the elastic stresses and pressure in the exit channel for all De. We provide analytical expressions for 111 112 the conformation tensor and the pressure drop in the high-Deborah-number limit, which are consistent with recent results of Hinch et al. (2023), thus complementing our previous 113 low-Deborah-number lubrication analysis (Boyko & Stone 2022). Furthermore, we analyze 114 the viscoelastic boundary layer near the walls at high Deborah numbers and derive the 115 boundary-layer asymptotic solutions. Given the well-known lack of accuracy and convergence 116 117 difficulties associated with the high-Weissenberg-number problem in numerical simulations (Owens & Phillips 2002; Alves et al. 2021), our analytical and semi-analytical results for the 118 119 ultra-dilute limit, valid at high Deborah numbers, are of fundamental importance as they may serve to validate simulation predictions or be compared with experimental measurements to 120 121 understand more about the applicability of model constitutive equations.

# 122 2. Problem formulation and governing equations

We analyze the incompressible steady flow of a viscoelastic fluid in a slowly varying and 123 124 symmetric two-dimensional contraction of height 2h(z) and length  $\ell$ , where  $h(z) \ll \ell$ , as illustrated in figure 1. Upstream of the contraction inlet (z = 0), there is an entry channel of 125 126 height  $2h_0$  and length  $\ell_0$ , and downstream of the contraction outlet  $(z = \ell)$ , there is an exit channel of height  $2h_{\ell}$  and length  $\ell_{\ell}$ . The fluid flow has velocity **u** and pressure distribution 127 p, which are induced by an imposed flow rate q (per unit depth). Our primary interest is 128 to determine the pressure drop  $\Delta p$  over the contraction region and the spatial relaxation of 129 pressure and elastic stresses in the exit channel. For our analysis, we shall employ two different 130 131 systems of coordinates. The first is the Cartesian coordinates (z, y) and  $(z_{\ell}, y)$ , where the z and  $z_{\ell} = z - \ell$  axes lie along the symmetry midplane of the channel (dashed-dotted line) and 132



FIGURE 1. Schematic illustration of the two-dimensional configuration consisting of a slowly varying and symmetric contraction of height 2h(z) and length  $\ell$  ( $h \ll \ell$ ). The contraction is connected to two long straight channels of height  $2h_0$  and  $2h_\ell$ , respectively, up- and downstream and contains a viscoelastic fluid steadily driven by the imposed flow rate q.

y is in the direction of the shortest dimension. The second one is the orthogonal curvilinear coordinates  $(\xi, \eta)$  defined in § 2.3.

We consider low-Reynolds-number flows so that the fluid motion is governed by the continuity equation and Cauchy momentum equations in the absence of inertia,

$$\nabla \cdot \boldsymbol{u} = 0, \qquad \nabla \cdot \boldsymbol{\sigma} = \boldsymbol{0}. \tag{2.1a, b}$$

To describe the viscoelastic behavior of the fluid, we use the Oldroyd-B constitutive model (Oldroyd 1950), which represents the most simple combination of viscous and elastic stresses and is used widely to describe the flow of viscoelastic Boger fluids, characterized by a constant shear viscosity. The Oldroyd-B equation can be derived from microscopic principles by modeling polymer molecules as elastic dumbbells, which follow a linear Hooke's law for the restoring force as they are advected and stretched by the flow. The corresponding stress tensor  $\sigma$  is

142

150

$$\boldsymbol{\sigma} = -p\boldsymbol{I} + 2\mu_s \boldsymbol{E} + \boldsymbol{\tau}_p, \tag{2.2}$$

where the first term on the right-hand side of (2.2) is the pressure contribution, the second term is the viscous stress contribution of a Newtonian solvent with a constant viscosity  $\mu_s$ , where  $\boldsymbol{E} = (\nabla \boldsymbol{u} + (\nabla \boldsymbol{u})^T)/2$  is the rate-of-strain tensor, and the last term,  $\tau_p$ , is the polymer contribution.

For the Oldroyd-B model, the polymer contribution to the stress tensor  $\tau_p$  can be expressed in terms of the (symmetric) conformation tensor (or the deformation of the microstructure) **A** as (Bird *et al.* 1987; Larson 1988; Morozov & Spagnolie 2015),

$$\boldsymbol{\tau}_p = G(\boldsymbol{A} - \boldsymbol{I}) = \frac{\mu_p}{\lambda} (\boldsymbol{A} - \boldsymbol{I}), \qquad (2.3)$$

where G is the elastic modulus,  $\lambda$  is the relaxation time, and  $\mu_p = G\lambda$  is the polymer contribution to the shear viscosity at zero shear rate. It is also convenient to introduce the total zero-shear-rate viscosity  $\mu_0 = \mu_s + \mu_p$ .

The evolution equation for the deformation of the microstructure **A** of the Oldroyd-B model fluid is given at steady state as (Bird *et al.* 1987; Larson 1988; Morozov & Spagnolie 2015)

157 
$$\boldsymbol{u} \cdot \boldsymbol{\nabla} \boldsymbol{A} - (\boldsymbol{\nabla} \boldsymbol{u})^{\mathrm{T}} \cdot \boldsymbol{A} - \boldsymbol{A} \cdot (\boldsymbol{\nabla} \boldsymbol{u}) = -\frac{1}{\lambda} (\boldsymbol{A} - \boldsymbol{I}). \qquad (2.4)$$

## 2.1. Scaling analysis and non-dimensionalization

We consider narrow configurations, in which  $h(z) \ll \ell$ ,  $h_0$  is the half-height at z = 0, and  $u_c = q/2h_0$  is the characteristic velocity scale set by the cross-sectionally averaged velocity. We introduce non-dimensional variables based on lubrication theory (Tichy 1996; Zhang

# Focus on Fluids articles must not exceed this page length

*et al.* 2002; Saprykin *et al.* 2007; Ahmed & Biancofiore 2021; Boyko & Stone 2022),

163 
$$Z = \frac{z}{\ell}, \qquad Y = \frac{y}{h_0}, \qquad U_z = \frac{u_z}{u_c}, \qquad U_y = \frac{u_y}{\epsilon u_c}, \qquad (2.5a)$$

164

165 
$$P = \frac{p}{\mu_0 u_c \ell / h_0^2}, \qquad \Delta P = \frac{\Delta p}{\mu_0 u_c \ell / h_0^2}, \qquad H = \frac{h}{h_0}, \qquad (2.5b)$$

166

167 
$$\tilde{A}_{zz} = \epsilon^2 A_{zz}, \qquad \tilde{A}_{zy} = \epsilon A_{zy}, \qquad \tilde{A}_{yy} = A_{yy}, \qquad (2.5c)$$

where we have introduced the aspect ratio of the configuration, which is assumed to be small,

169 
$$\epsilon = \frac{h_0}{\ell} \ll 1, \tag{2.6}$$

170 the contraction ratio,

$$H_{\ell} = \frac{h_{\ell}}{h_0},\tag{2.7}$$

172 the viscosity ratios,

173 
$$\tilde{\beta} = \frac{\mu_p}{\mu_s + \mu_p} = \frac{\mu_p}{\mu_0} \text{ and } \beta = 1 - \tilde{\beta} = \frac{\mu_s}{\mu_0},$$
 (2.8)

and the Deborah and Weissenberg numbers,

175 
$$De = \frac{\lambda u_c}{\ell}$$
 and  $Wi = \frac{\lambda u_c}{h_0}$ . (2.9)

For lubrication flows through narrow geometries that we consider, there is a difference 176 between the Deborah and Weissenberg numbers because of the two distinct length scales. 177 178 The Weissenberg number Wi is the product of the relaxation time scale of the fluid,  $\lambda$ , and the characteristic shear rate of the flow,  $h_0/u_c$ . On the other hand, the Deborah number De 179 is the ratio of the relaxation time,  $\lambda$ , to the residence time in the contraction region,  $\ell/u_c$ , or 180 alternatively, the product of the relaxation time and the characteristic extensional rate of the 181 flow (Tichy 1996; Zhang et al. 2002; Saprykin et al. 2007; Ahmed & Biancofiore 2021). The 182 183 Deborah and Weissenberg numbers are related through  $De = \epsilon Wi$ , and for narrow geometries with  $\epsilon \ll 1$ , *De* can be small while keeping Wi = O(1). 184

Similar to our previous study (Boyko & Stone 2022), we non-dimensionalize the pressure 185 using the total zero-shear-rate viscosity  $\mu_0 = \mu_s + \mu_p$ . However, for convenience, we non-186 dimensionalize the height based on the entry height rather than the exit height. In addition, 187 unlike our previous study, we do not scale the deformation of the microstructure with  $De^{-1}$ . 188 Our current scaling is consistent with a fully developed unidirectional flow of an Oldroyd-B 189 fluid in a straight channel, which yields  $\tilde{A}_{zz} = O(De^2)$ ,  $\tilde{A}_{zy} = O(De)$ , and  $\tilde{A}_{yy} = O(1)$ ; see 190 (2.10d) –(2.10f) and (2.16). This scaling is convenient when considering arbitrary and large 191 192 values of the Deborah number.

Note that in both Hinch *et al.* (2023) and here, the channel height is 2h, but the total flow rate per unit depth in the former is 2q, whereas in this work it is q as in Boyko & Stone (2022). All results are compatible because the variables used for the non-dimensionalization are the same, i.e., the expressions for the characteristic velocity, characteristic pressure, and the Deborah number are the same.



FIGURE 2. Schematic illustration of the orthogonal curvilinear coordinates ( $\xi$ ,  $\eta$ ) for a slowly varying geometry. The coordinate  $\xi$  is constant along vertical grid lines, and  $\eta$ , defined in (2.11), is constant along the curves going from left to right.

# 2.2. Dimensionless lubrication equations in Cartesian coordinates

Using the non-dimensionalization (2.5)–(2.9), to the leading order in  $\epsilon$ , the governing equations (2.1)–(2.4) take the form

201 
$$\frac{\partial U_z}{\partial Z} + \frac{\partial U_y}{\partial Y} = 0, \qquad (2.10a)$$

202

226

198

203  
204
$$\frac{\partial P}{\partial Z} = (1 - \tilde{\beta}) \frac{\partial^2 U_z}{\partial Y^2} + \frac{\tilde{\beta}}{De} \left( \frac{\partial \tilde{A}_{zz}}{\partial Z} + \frac{\partial \tilde{A}_{zy}}{\partial Y} \right), \quad (2.10b)$$

$$\frac{\partial P}{\partial V} = 0, \qquad (2.10c)$$

$$\frac{205}{206} \qquad \qquad \partial Y = 0, \tag{2.10}$$

$$U_{z}\frac{\partial\tilde{A}_{zz}}{\partial Z} + U_{y}\frac{\partial\tilde{A}_{zz}}{\partial Y} - 2\frac{\partial U_{z}}{\partial Z}\tilde{A}_{zz} - 2\frac{\partial U_{z}}{\partial Y}\tilde{A}_{zy} = -\frac{1}{De}\tilde{A}_{zz}, \qquad (2.10d)$$

$$U_{z}\frac{\partial\tilde{A}_{zy}}{\partial Z} + U_{y}\frac{\partial\tilde{A}_{zy}}{\partial Y} - \frac{\partial U_{y}}{\partial Z}\tilde{A}_{zz} - \frac{\partial U_{z}}{\partial Y}\tilde{A}_{yy} = -\frac{1}{De}\tilde{A}_{zy}, \qquad (2.10e)$$

211 
$$U_{z}\frac{\partial \tilde{A}_{yy}}{\partial Z} + U_{y}\frac{\partial \tilde{A}_{yy}}{\partial Y} - 2\frac{\partial U_{y}}{\partial Z}\tilde{A}_{zy} - 2\frac{\partial U_{y}}{\partial Y}\tilde{A}_{yy} = -\frac{1}{De}(\tilde{A}_{yy} - 1).$$
(2.10f)

From (2.10*c*), it follows that P = P(Z), i.e., the pressure is independent of Y up to  $O(\epsilon^2)$ , consistent with the classical lubrication approximation. We note that the scaled  $\tilde{A}_{zz}$  on the right-hand side of (2.10*d*) relaxes to  $\epsilon^2$ , which is neglected at the leading order in  $\epsilon$ .

# 215 2.3. Orthogonal curvilinear coordinates for a slowly varying geometry

For our theoretical analysis, it is convenient to transform the geometry of the contraction from the Cartesian coordinates (Z, Y) to curvilinear coordinates  $(\xi, \eta)$ , as illustrated in figure 2, with the mapping (Hinch *et al.* 2023),

219 
$$\xi = Z - \frac{1}{2}\epsilon^2 \frac{H'(Z)}{H(Z)} (H(Z)^2 - Y^2) + O(\epsilon^4), \qquad \eta = \frac{Y}{H(Z)}.$$
 (2.11)

As shown in appendix **A**, the curvilinear coordinates  $(\xi, \eta)$  are orthogonal with a relative error of  $O(\epsilon^4)$ , i.e.,  $\nabla \xi \cdot \nabla \eta = O(\epsilon^4)$ .

Hereafter, we use  $\mathbf{u} = u\mathbf{e}_{\xi} + v\mathbf{e}_{\eta}$  and  $\mathbf{A} = A_{11}\mathbf{e}_{\xi}\mathbf{e}_{\xi} + A_{12}(\mathbf{e}_{\xi}\mathbf{e}_{\eta} + \mathbf{e}_{\eta}\mathbf{e}_{\xi}) + A_{22}\mathbf{e}_{\eta}\mathbf{e}_{\eta}$  to denote, respectively, the components of velocity and deformation of the microstructure in the curvilinear coordinates  $(\xi, \eta)$ . The corresponding non-dimensional velocity components in different coordinates are related through (see appendix A)

$$U_z = U - \epsilon^2 \eta H'(\xi) V, \qquad U_y = \eta H'(\xi) U + V.$$
 (2.12)

$$\tilde{A}_{zz} = \tilde{A}_{11} + O(\epsilon^2), \qquad (2.13a)$$

$$\tilde{A}_{zy} = \tilde{A}_{12} + \eta H'(\xi) \tilde{A}_{11} + O(\epsilon^2), \qquad (2.13b)$$

233 
$$\tilde{A}_{yy} = \tilde{A}_{22} + 2\eta H'(\xi) \tilde{A}_{12} + \eta^2 (H'(\xi))^2 \tilde{A}_{11} + O(\epsilon^2).$$
(2.13c)

Finally, we note that since there is only a  $O(\epsilon^2)$  difference between the  $\xi$ - and z-directions, 234 for convenience, we continue to use Z rather than  $\xi$  in curvilinear coordinates. 235

#### 2.4. Dimensionless lubrication equations in orthogonal curvilinear coordinates 236

Using the mapping (2.11), the governing equations (2.10) take the form in the curvilinear 237 coordinates (Hinch et al. 2023), 238

239 
$$\frac{\partial(HU)}{\partial Z} + \frac{\partial V}{\partial \eta} = 0, \qquad (2.14a)$$

240

$$\frac{\mathrm{d}P}{\mathrm{d}Z} = (1 - \tilde{\beta})\frac{1}{H^2}\frac{\partial^2 U}{\partial\eta^2} + \frac{\tilde{\beta}}{De}\left(\frac{1}{H}\frac{\partial(H\tilde{A}_{11})}{\partial Z} + \frac{1}{H}\frac{\partial\tilde{A}_{12}}{\partial\eta}\right),\tag{2.14b}$$

243  
244 
$$U\frac{\partial \tilde{A}_{11}}{\partial Z} + \frac{V}{H}\frac{\partial \tilde{A}_{11}}{\partial \eta} - 2\frac{\partial U}{\partial Z}\tilde{A}_{11} - \frac{2}{H}\frac{\partial U}{\partial \eta}\tilde{A}_{12} = -\frac{1}{De}\tilde{A}_{11}, \qquad (2.14c)$$

$$U\frac{\partial\tilde{A}_{12}}{\partial Z} + \frac{V}{H}\frac{\partial\tilde{A}_{12}}{\partial \eta} - H\frac{\partial}{\partial Z}\left(\frac{V}{H}\right)\tilde{A}_{11} - \frac{1}{H}\frac{\partial U}{\partial \eta}\tilde{A}_{22} = -\frac{1}{De}\tilde{A}_{12}, \qquad (2.14d)$$

246

247 
$$U\frac{\partial \tilde{A}_{22}}{\partial Z} + \frac{V}{H}\frac{\partial \tilde{A}_{22}}{\partial \eta} - 2H\frac{\partial}{\partial Z}\left(\frac{V}{H}\right)\tilde{A}_{12} + 2\frac{\partial U}{\partial Z}\tilde{A}_{22} = -\frac{1}{De}(\tilde{A}_{22} - 1).$$
(2.14e)

The corresponding boundary conditions on the velocity are

$$U(Z,1) = 0, \quad V(Z,1) = 0, \quad \frac{\partial U}{\partial \eta}(Z,0) = 0, \quad H(Z) \int_0^1 U(Z,\eta) d\eta = 1, \quad (2.15a - d)$$

which represent, respectively, the no-slip and no-penetration boundary conditions along the channel walls, the symmetry boundary condition at the centerline, and the integral mass conservation along the channel. In addition, we assume a fully developed unidirectional Poiseuille flow in the straight entry channel and the corresponding deformation of the microstructure,

$$\tilde{A}_{11} = \frac{18De^2}{H^4}\eta^2, \qquad \tilde{A}_{12} = -\frac{3De}{H^2}\eta, \qquad \tilde{A}_{22} = 1,$$
 (2.16*a* - *c*)

248 with  $H \equiv 1$  at the entrance. We also assume that far downstream in the exit channel, the deformation of the microstructure attains a fully relaxed value, given by (2.16) with  $H \equiv H_{\ell}$ . 249

#### 2.5. Pressure drop across the non-uniform region in the lubrication limit 250

In this subsection, we show that one can calculate the pressure drop without solving directly 251 for the velocity field. To this end, we first integrate by parts the integral constraint (2.15d), 252 repeatedly, using (2.15*a*) and (2.15*c*), e.g., (Hinch *et al.* 2023), 253

254 
$$\frac{1}{H(Z)} = \int_0^1 U d\eta = \underbrace{\eta U|_0^1}_{0} - \int_0^1 \eta \frac{\partial U}{\partial \eta} d\eta = \underbrace{\frac{1}{2}(1-\eta^2)\frac{\partial U}{\partial \eta}|_0^1}_{0} - \frac{1}{2}\int_0^1 (1-\eta^2)\frac{\partial^2 U}{\partial \eta^2} d\eta. \quad (2.17)$$

255 Substituting the expression for  $\partial^2 U/\partial \eta^2$  from (2.14b) into (2.17), we obtain

256 
$$-\frac{1-\tilde{\beta}}{H(Z)^3} = \frac{1}{2} \int_0^1 (1-\eta^2) \left[ \frac{\mathrm{d}P}{\mathrm{d}Z} - \frac{\tilde{\beta}}{De} \left( \frac{1}{H} \frac{\partial(H\tilde{A}_{11})}{\partial Z} + \frac{1}{H} \frac{\partial\tilde{A}_{12}}{\partial \eta} \right) \right] \mathrm{d}\eta, \qquad (2.18)$$

which can be rearranged to yield the pressure gradient,

258 
$$\frac{\mathrm{d}P}{\mathrm{d}Z} = -\frac{3(1-\tilde{\beta})}{H(Z)^3} + \frac{3\tilde{\beta}}{2De} \int_0^1 (1-\eta^2) \left[ \frac{1}{H(Z)} \frac{\partial(H(Z)\tilde{A}_{11})}{\partial Z} + \frac{1}{H(Z)} \frac{\partial\tilde{A}_{12}}{\partial \eta} \right] \mathrm{d}\eta. \quad (2.19)$$

Integrating (2.19) with respect to Z from 0 to 1 provides the pressure drop  $\Delta P = P(0) - P(1)$ across the *non-uniform region*,

261 
$$\Delta P = 3(1 - \tilde{\beta}) \int_0^1 \frac{dZ}{H(Z)^3}$$

262 
$$-\frac{3\tilde{\beta}}{2De}\int_{0}^{1}\int_{0}^{1}(1-\eta^{2})\left[\frac{1}{H(Z)}\frac{\partial(H(Z)\tilde{A}_{11})}{\partial Z}+\frac{1}{H(Z)}\frac{\partial\tilde{A}_{12}}{\partial\eta}\right]d\eta dZ. \quad (2.20)$$

Using integration by parts, (2.20) can be expressed as

264 
$$\Delta P = 3(1 - \tilde{\beta}) \int_{0}^{1} \frac{dZ}{H(Z)^{3}} + \frac{3\tilde{\beta}}{2De} \int_{0}^{1} (1 - \eta^{2}) \left[ \tilde{A}_{11}(0, \eta) - \tilde{A}_{11}(1, \eta) \right] d\eta$$
  
$$3\tilde{\beta} \int_{0}^{1} \left[ \frac{H'(Z)}{L} \int_{0}^{1} (1 - \eta^{2}) \left[ \tilde{A}_{11}(0, \eta) - \tilde{A}_{11}(1, \eta) \right] d\eta$$

265 
$$-\frac{3\tilde{\beta}}{2De}\int_{0}^{1}\left[\frac{H'(Z)}{H(Z)}\left(\int_{0}^{1}(1-\eta^{2})\tilde{A}_{11}d\eta\right)\right]dZ - \frac{3\tilde{\beta}}{De}\int_{0}^{1}\left[\frac{1}{H(Z)}\int_{0}^{1}\eta\tilde{A}_{12}d\eta\right]dZ, (2.21)$$

where prime indicates a derivative with respect to Z.

Equation (2.21) resembles the result of an application of the reciprocal theorem previously 267 derived for the pressure drop of the flow of an Oldroyd-B fluid in a slowly varying 268 channel (Boyko & Stone 2021, 2022). The first term on the right-hand side of (2.21) 269 represents the viscous contribution of the Newtonian solvent to the pressure drop. The 270 second term represents the contribution of the elastic normal stress difference at the inlet 271 and outlet of the non-uniform channel. The third term represents the contribution of the 272 elastic normal stresses that arise due to the spatial variations in the channel shape, which is 273 a contribution that is absent in a straight channel. Finally, the last term represents the elastic 274 275 contribution due to shear stresses within the fluid domain of the non-uniform channel. It should be noted that we do not assume a priori the particular shape of the channel H(Z) but 276 rather consider a flow in a slowly varying channel of arbitrary shape H(Z). 277

# 278 **3.** Low- $\tilde{\beta}$ lubrication analysis in a slowly varying region

In the previous section, we obtained the dimensionless equations (2.14), which are governed by the two non-dimensional parameters,  $\tilde{\beta}$  and De, in the lubrication limit ( $\epsilon \ll 1$ ). In this section, we derive analytical expressions for the velocity, conformation tensor, and the  $q - \Delta p$  relation for the pressure-driven flow of a very dilute viscoelastic Oldroyd-B fluid,  $\tilde{\beta} = \mu_p/\mu_0 \ll 1$  in a slowly varying channel of arbitrary shape H(Z).

In contrast to our previous study that employed a low-Deborah-number lubrication analysis (Boyko & Stone 2022), in this work, we assume De = O(1) and consider the ultra-dilute limit,  $\tilde{\beta} \ll 1$  (see Remmelgas *et al.* 1999; Moore & Shelley 2012; Li *et al.* 2019;

8

287 Mokhtari et al. 2022). To this end, we seek solutions of the form

$$\begin{pmatrix} U \\ V \\ P \\ \tilde{A}_{11} \\ \tilde{A}_{12} \\ \tilde{A}_{22} \end{pmatrix} = \begin{pmatrix} U_0 \\ V_0 \\ P_0 \\ \tilde{A}_{11,0} \\ \tilde{A}_{12,0} \\ \tilde{A}_{22,0} \end{pmatrix} + \tilde{\beta} \begin{pmatrix} U_1 \\ V_1 \\ P_1 \\ \tilde{A}_{11,1} \\ \tilde{A}_{12,1} \\ \tilde{A}_{12,1} \\ \tilde{A}_{22,1} \end{pmatrix} + O(\epsilon^2, \tilde{\beta}^2).$$
(3.1)

288

299

301

The ultra-dilute limit represents a one-way coupling between the velocity and pressure fields and the deformation of the microstructure (polymer stresses or conformation tensor). At leading order, the velocity and pressure are Newtonian, and the deformation of the microstructure (i.e., polymer stresses) arises from this Newtonian flow. Accordingly, the velocity and pressure at  $O(\tilde{\beta})$  arise due to leading-order polymer stresses. In the next subsections, we provide closed-form asymptotic expressions for the velocity field and conformation tensor components at  $O(\tilde{\beta}^0)$  and the pressure drop up to  $O(\tilde{\beta})$ .

We note that the viscosity ratio  $\tilde{\beta} = \mu_p/\mu_0$  is related to the so-called concentration of the polymers  $c = \mu_p/\mu_s$  through  $\tilde{\beta} = c/(c+1)$ . Thus, at the leading order, the limits  $\tilde{\beta} \ll 1$  and  $c \ll 1$  are identical.

# 3.1. Velocity, conformation, and pressure drop at the leading order in $\tilde{\beta}$

Substituting (3.1) into (2.14*a*)–(2.14*b*) and considering the leading order in  $\tilde{\beta}$ , the continuity and momentum equations take the form

$$\frac{\partial (HU_0)}{\partial Z} + \frac{\partial V_0}{\partial \eta} = 0 \qquad \text{and} \qquad \frac{\mathrm{d}P_0}{\mathrm{d}Z} = \frac{1}{H^2} \frac{\partial^2 U_0}{\partial \eta^2}, \qquad (3.2a, b)$$

subject to the boundary conditions

$$U_0(Z,1) = 0, \quad V_0(Z,1) = 0, \quad \frac{\partial U_0}{\partial \eta}(Z,0) = 0, \quad H(Z) \int_0^1 U_0(Z,\eta) d\eta = 1. \quad (3.3a-d)$$

The solutions for the axial velocity  $U_0$  and the pressure drop  $\Delta P_0$  at the leading order are well-known (see, e.g., Boyko & Stone 2022)

$$U_0 = \frac{3}{2} \frac{1}{H(Z)} (1 - \eta^2)$$
 and  $\Delta P_0 = 3 \int_0^1 \frac{dZ}{H(Z)^3}$ . (3.4*a*, *b*)

Substituting (3.4a) into the continuity equation (3.2a) and using (3.3b), yields

$$V_0 \equiv 0. \tag{3.5}$$

From (3.5), it follows that in the orthogonal curvilinear coordinates, the velocity in the  $\eta$ -direction is identically zero at  $O(\tilde{\beta}^0)$ , in contrast to the Cartesian coordinates where  $U_{y,0} = (3/2)H'(Z)Y(H(Z)^2 - Y^2)/H(Z)^4$ . As we shall see, this fact significantly simplifies the theoretical analysis and allows us to derive closed-form expressions for the components of the conformation tensor.

Using (3.5), at leading order in  $\tilde{\beta}$ , the equations for the conformation tensor components, (2.14*c*)–(2.14*e*), simplify to

309  
310  

$$U_0 \frac{\partial A_{22,0}}{\partial Z} + 2 \frac{\partial U_0}{\partial Z} \tilde{A}_{22,0} = -\frac{1}{De} (\tilde{A}_{22,0} - 1), \qquad (3.6a)$$

311 
$$U_0 \frac{\partial A_{12,0}}{\partial Z} - \frac{1}{H} \frac{\partial U_0}{\partial \eta} \tilde{A}_{22,0} = -\frac{1}{De} \tilde{A}_{12,0}, \qquad (3.6b)$$

E. Boyko, E.J. Hinch and H.A. Stone

10

$$U_0 \frac{\partial \tilde{A}_{11,0}}{\partial Z} - 2 \frac{\partial U_0}{\partial Z} \tilde{A}_{11,0} - \frac{2}{H} \frac{\partial U_0}{\partial \eta} \tilde{A}_{12,0} = -\frac{1}{De} \tilde{A}_{11,0}, \qquad (3.6c)$$

subject to the boundary conditions

$$\tilde{A}_{11,0}(0,\eta) = 18De^2\eta^2, \qquad \tilde{A}_{12,0}(0,\eta) = -3De\eta, \qquad \tilde{A}_{22,0}(0,\eta) = 1.$$
 (3.7*a* - *c*)

Equations (3.6) represent a set of one-way coupled first-order semi-linear partial differential 313 equations that can be solved first for  $\tilde{A}_{22,0}$ , followed by  $\tilde{A}_{12,0}$ , and then for  $\tilde{A}_{11,0}$ . 314

Solving (3.6) together with (3.7), we obtain closed-form expressions for  $\tilde{A}_{22,0}$ ,  $\tilde{A}_{12,0}$ , and 315  $\tilde{A}_{11,0}$  for arbitrary values of *De* and the shape function H(Z), 316

317 
$$\frac{\tilde{A}_{22,0}}{H(Z)^2} = e^{f(DeU_0(Z,\eta))} \left[ 1 + \int_0^Z e^{-f(DeU_0(\tilde{Z},\eta))} \frac{1}{DeU_0(\tilde{Z},\eta)H(\tilde{Z})^2} d\tilde{Z} \right],$$
(3.8)

$$\frac{\tilde{A}_{12,0}}{(-3De\eta)} = e^{f(DeU_0(Z,\eta))} \left[ 1 + \int_0^Z e^{-f(DeU_0(\tilde{Z},\eta))} \frac{\tilde{A}_{22,0}(\tilde{Z},\eta)}{DeU_0(\tilde{Z},\eta)H(\tilde{Z})^2} d\tilde{Z} \right],$$
(3.9)

$$\frac{\tilde{A}_{11,0}}{18De^2\eta^2/H(Z)^2} = e^{f(DeU_0(Z,\eta))} \left[ 1 + \int_0^Z e^{-f(DeU_0(\tilde{Z},\eta))} \frac{\tilde{A}_{12,0}(\tilde{Z},\eta)}{(-3\eta De)DeU_0(\tilde{Z},\eta)} d\tilde{Z} \right],$$
(3.10)

321

where  $f(DeU_0(Z,\eta))$  is defined as 322

323 
$$f(DeU_0(Z,\eta)) = -\int_0^Z \frac{1}{DeU_0(\tilde{Z},\eta)} d\tilde{Z} = -\int_0^Z \frac{2H(\tilde{Z})}{3De(1-\eta^2)} d\tilde{Z}.$$
 (3.11)

It is worth noting that the right-hand side of (3.8)–(3.10) depends on the product  $DeU_0(Z, \eta)$ 324 325 and are not functions of De and  $\eta$  separately. Furthermore, (3.8)–(3.10) clearly show that while the distribution of  $\tilde{A}_{22,0}$  is set solely by the value at the beginning of the non-uniform 326 region, the distribution of elastic shear and normal stresses,  $\tilde{A}_{12,0}$  and  $\tilde{A}_{11,0}$ , are coupled to 327 the transverse normal stress  $\tilde{A}_{22,0}$ . In fact, the elastic normal stress  $\tilde{A}_{11,0}$  depends both on 328  $\tilde{A}_{12,0}$  and  $\tilde{A}_{22,0}$ . 329

From (3.8)–(3.10), one might think that the conformation tensor components diverge at 330 the wall  $(\eta = \pm 1)$ . However, using (3.6) and noting that  $U_0 = \partial U_0 / \partial Z = 0$  at  $\eta = \pm 1$ , it 331 follows that at the walls of the non-uniform channel, 332

333 
$$\tilde{A}_{22,0}^{\text{wall}} = 1, \qquad \tilde{A}_{12,0}^{\text{wall}} = \mp \frac{3De}{H(Z)^2}, \qquad \tilde{A}_{11,0}^{\text{wall}} = \frac{18De^2}{H(Z)^4} \quad \text{for all } De.$$
(3.12)

In §§ 3.1.1 and 3.1.2, we provide explicit expressions for the conformation tensor components 334 in the low- and high-De limits. We also note that the results shown in our figure 4(a, c) and 335 the work of Hinch et al. (2023) suggest the existence of a viscoelastic boundary layer near 336 the walls in the high-De limit, which we analyze in § 3.1.3. 337

#### 338 3.1.1. Conformation tensor in the low-De limit

For  $De \ll 1$ , we solve the equations iteratively for the conformation tensor components (3.6) 339 to obtain 340

341 
$$\tilde{A}_{22,0} = 1 + \frac{3DeH'}{H^2}(1-\eta^2) + \frac{9De^2[4H'^2 - HH'']}{2H^4}(1-\eta^2)^2$$

$$+ \frac{27De^{3}[24H'^{3} - 13HH'H'' + H^{2}H''']}{4H^{6}}(1 - \eta^{2})^{3}, \qquad (3.13a)$$

344 
$$\tilde{A}_{12,0} = -\frac{3De}{H^2}\eta - \frac{18De^2H'}{H^4}\eta(1-\eta^2) - \frac{81De^3[4H'^2 - HH'']}{2H^6}\eta(1-\eta^2)^2, \quad (3.13b)$$

# Rapids articles must not exceed this page length

345 
$$\tilde{A}_{11,0} = \frac{18De^2}{H^4}\eta^2 + \frac{162De^3H'}{H^6}\eta^2(1-\eta^2) + \frac{486De^4[4H'^2 - HH'']}{H^8}\eta^2(1-\eta^2)^2. \quad (3.13c)$$

We note that the low-*De* results (3.13) are consistent with our previous work (Boyko & Stone 2022), in which we provided explicit expressions for  $\tilde{A}_{zz}$ ,  $\tilde{A}_{zy}$ , and  $\tilde{A}_{yy}$  up to  $O(De^2)$ in Cartesian coordinates. For example, using (2.13*c*) and (3.13),  $\tilde{A}_{yy}$  can be expressed as  $\tilde{A}_{yy} = 1 + 3DeH'(Z)(H(Z)^2 - 3Y^2)/H(Z)^4 + O(De^2)$ , in agreement with (3.9*a*) in Boyko & Stone (2022).

# 351 3.1.2. Conformation tensor in the high-De limit

We here provide the closed-form expressions for the conformation tensor components in the high-*De* limit. We begin with the expression for  $\tilde{A}_{22,0}$  and consider the core flow region.

For  $De \gg 1$ , except close to the wall, (3.6*a*) reduces to

355 
$$U_0 \frac{\partial \tilde{A}_{22,0}}{\partial Z} + 2 \frac{\partial U_0}{\partial Z} \tilde{A}_{22,0} = 0, \qquad (3.14)$$

356 whose solution subject to (3.7c) is

357 
$$\tilde{A}_{22,0}(Z,\eta) = \tilde{A}_{22,0}(0,\eta) \frac{U_0(0,\eta)^2}{U_0(Z,\eta)^2} = H(Z)^2.$$
(3.15)

Next, since  $\tilde{A}_{12,0}$  scales as O(De) while  $\tilde{A}_{22,0}$  is O(1), within the core flow region in the high-*De* limit we obtain that the first term in (3.6*b*) dominates over all the remaining terms,

360 
$$U_0 \frac{\partial \tilde{A}_{12,0}}{\partial Z} = 0, \qquad (3.16)$$

so that elastic shear stresses preserve their value from the entry channel through the nonuniform region,

$$\tilde{A}_{12,0}(Z,\eta) = \tilde{A}_{12,0}(0,\eta) = -3De\eta.$$
(3.17)

Finally, to determine  $A_{11,0}$ , we note that the third and fourth terms in (3.6*c*) scale as O(De), while the first and second terms are  $O(De^2)$ . Thus, for  $De \gg 1$ , we expect the first and second terms to balance each other while the remaining terms are negligible, so that

367 
$$U_0 \frac{\partial A_{11,0}}{\partial Z} - 2 \frac{\partial U_0}{\partial Z} \tilde{A}_{11,0} = 0.$$
(3.18)

368 Solving (3.18) subject to (3.7a) yields

363

369 
$$\tilde{A}_{11,0}(Z,\eta) = \tilde{A}_{11,0}(0,\eta) \frac{U_0(Z,\eta)^2}{U_0(0,\eta)^2} = \frac{18De^2\eta^2}{H(Z)^2}.$$
 (3.19)

In fact, for  $De \gg 1$ , there is a purely passive response of the microstructure, similar to a material line-element, transported and deformed by the flow without relaxing.

The high-*De* results (3.15), (3.17), and (3.19) can be also directly obtained from the closed-form solutions (3.8)–(3.10) by noting that for  $De \gg 1$ ,  $e^{\pm f(DeU_0(Z,\eta))} \approx 1$ , and neglecting the  $O(De^{-1})$  terms.

## 375 3.1.3. Boundary-layer analysis in the high-De limit

In the previous section, we obtained analytical expressions for the components of the conformation tensor in the high-*De* limit within the core flow region. However, these expressions do not hold near the walls, where a viscoelastic boundary layer of  $O(De^{-1})$ thickness exists (Hinch *et al.* 2023). In this section, we analyze this boundary-layer region 380 and provide boundary-layer equations and their closed-form solutions. To this end, we focus on the region,  $\eta \in [0, 1]$ , and introduce the rescaled inner-region coordinate 381

$$\zeta = De(1 - \eta) = De\tilde{\eta} \quad \text{for} \quad \tilde{\eta} \ll 1, \tag{3.20}$$

so that  $De(1 - \eta^2) = \zeta(2 - \tilde{\eta}) \approx 2\zeta$ . Noting that in the boundary layer,  $\tilde{A}_{22,0} = O(1)$ ,  $\tilde{A}_{12,0} = O(De)$ , and  $\tilde{A}_{11,0} = O(De^2)$  (see (3.12)), to eliminate the dependence on De in 383 384 the governing equations and boundary conditions (3.7), we rescale  $\tilde{A}_{22,0}$ ,  $\tilde{A}_{12,0}$ , and  $\tilde{A}_{11,0}$ , 385 which are functions of Z and  $\zeta$ , as 386

387 
$$\mathcal{A}_{22} = \frac{\tilde{A}_{22,0}}{H(Z)^2}, \qquad \mathcal{A}_{12} = \frac{\tilde{A}_{12,0}}{(-3\eta De)}, \qquad \mathcal{A}_{11} = \frac{\tilde{A}_{11,0}}{18\eta^2 De^2/H(Z)^2}.$$
 (3.21)

Substituting (3.20) and (3.21) into (3.6) and using (3.4a), we obtain the boundary-layer 388 equations in the high-De limit, 389

$$\frac{3\zeta}{H(Z)}\frac{\partial\mathcal{A}_{22}}{\partial Z} = -\left(\mathcal{A}_{22} - \frac{1}{H(Z)^2}\right),\tag{3.22a}$$

$$\frac{3\zeta}{H(Z)}\frac{\partial\mathcal{A}_{12}}{\partial Z} = -(\mathcal{A}_{12} - \mathcal{A}_{22}), \qquad (3.22b)$$

$$\frac{3\zeta}{H(Z)}\frac{\partial\mathcal{A}_{11}}{\partial Z} = -(\mathcal{A}_{11} - \mathcal{A}_{12}), \qquad (3.22c)$$

subject to the inlet conditions

$$\mathcal{A}_{11}(0,\zeta) = 1, \qquad \mathcal{A}_{12}(0,\zeta) = 1, \qquad \mathcal{A}_{22}(0,\zeta) = 1.$$
 (3.23*a* - *c*)

Solving (3.22) together with (3.23), we obtain closed-form expressions for  $\mathcal{A}_{22}$ ,  $\mathcal{A}_{12}$ , and 395  $\mathcal{A}_{11}$  in the boundary-layer region 396

397 
$$\mathcal{A}_{22} = e^{\mathcal{F}(Z,\zeta)} \left[ 1 + \int_0^Z e^{-\mathcal{F}(\tilde{Z},\zeta)} \frac{1}{3\zeta H(\tilde{Z})} d\tilde{Z} \right], \qquad (3.24a)$$

398

407

394

399 
$$\mathcal{A}_{12} = e^{\mathcal{F}(Z,\zeta)} \left[ 1 + \int_0^Z e^{-\mathcal{F}(\tilde{Z},\zeta)} \frac{\mathcal{A}_{22}(\tilde{Z},\zeta)H(\tilde{Z})}{3\zeta} d\tilde{Z} \right], \qquad (3.24b)$$

401 
$$\mathcal{A}_{11} = e^{\mathcal{F}(Z,\zeta)} \left[ 1 + \int_0^Z e^{-\mathcal{F}(\tilde{Z},\zeta)} \frac{\mathcal{A}_{12}(\tilde{Z},\zeta)H(\tilde{Z})}{3\zeta} d\tilde{Z} \right], \qquad (3.24c)$$

where  $\mathcal{F}(Z, \zeta)$  is defined as 402

403 
$$\mathcal{F}(Z,\zeta) = -\frac{1}{3\zeta} \int_0^Z H(\tilde{Z}) d\tilde{Z}.$$
 (3.25)

We note that solutions (3.24) satisfy the matching conditions between the inner 404 and outer regions. Specifically,  $\mathcal{A}_{22}|_{\zeta \to \infty} = \left[\tilde{A}_{22,0}^{\text{core}}/H(Z)^2\right]_{\eta=1} = 1, \ \mathcal{A}_{12}|_{\zeta \to \infty} =$ 405  $\left[\tilde{A}_{12,0}^{\text{core}}/(-3\eta De)\right]_{\eta=1} = 1, \text{ and } \mathcal{A}_{11}|_{\zeta \to \infty} = \left[\tilde{A}_{11,0}^{\text{core}}/(18\eta^2 De^2/H(Z)^2)\right]_{\eta=1} = 1.$ 406

# 3.2. Pressure drop at the first order in $\tilde{\beta}$

Equation (2.20) shows that the pressure drop depends on the elastic normal and shear stresses 408  $\tilde{A}_{11}$  and  $\tilde{A}_{12}$ , and thus, generally, requires the solution of the nonlinear viscoelastic problem. 409

However, in the ultra-dilute limit, corresponding to  $\tilde{\beta} = \mu_p/\mu_0 \ll 1$ , we can determine the 410

12

382

pressure drop at  $O(\tilde{\beta})$  for arbitrary values of *De* only with the knowledge of the velocity 411 field and conformation tensor components at O(1). Specifically, substituting (3.1) into (2.20) 412

yields at  $O(\tilde{\beta})$  the pressure drop  $\Delta P_1$ , 413

422

414 
$$\Delta P_{1} = -3 \int_{0}^{1} \frac{dZ}{H(Z)^{3}}$$
415 
$$-\frac{3}{2De} \int_{0}^{1} \int_{0}^{1} (1 - \eta^{2}) \left[ \frac{1}{H(Z)} \frac{\partial (H(Z)\tilde{A}_{11,0})}{\partial Z} + \frac{1}{H(Z)} \frac{\partial \tilde{A}_{12,0}}{\partial \eta} \right] d\eta dZ, (3.26)$$

or alternatively, 416

417 
$$\Delta P_1 = -3 \int_0^1 \frac{\mathrm{d}Z}{H(Z)^3} + \frac{3}{2De} \int_0^1 (1 - \eta^2) \left[ \tilde{A}_{11,0}(0,\eta) - \tilde{A}_{11,0}(1,\eta) \right] \mathrm{d}\eta$$
  
3  $\int_0^1 \left[ \frac{H'(Z)}{H(Z)} \left( \int_0^1 (1 - \eta^2) \left[ \tilde{A}_{11,0}(0,\eta) - \tilde{A}_{11,0}(1,\eta) \right] \right] \mathrm{d}\eta$ 

418 
$$-\frac{3}{2De}\int_{0}^{1}\left[\frac{H'(Z)}{H(Z)}\left(\int_{0}^{1}(1-\eta^{2})\tilde{A}_{11,0}d\eta\right)\right]dZ - \frac{3}{De}\int_{0}^{1}\left[\frac{1}{H(Z)}\int_{0}^{1}\eta\tilde{A}_{12,0}d\eta\right]dZ$$
(3.27)

Thus, for a given flow rate q, the dimensionless pressure drop  $\Delta P = \Delta p / (\mu_0 q \ell / 2h_0^3)$ , as a 419 function of the shape function H(Z), the Deborah number De, and the viscosity ratio  $\tilde{\beta} \ll 1$ , 420 up to  $O(\tilde{\beta})$ , is given by 421

$$\Delta P = \Delta P_0(H(Z)) + \tilde{\beta} \Delta P_1(De, H(Z)) + O(\epsilon^2, \tilde{\beta}^2), \qquad (3.28)$$

where the expressions for  $\Delta P_0$  and  $\Delta P_1$  are given in (3.4b) and (3.27), respectively. 423

Notably, in contrast to our previous results for the pressure drop obtained in the weakly 424 viscoelastic and lubrication limits with  $De \ll 1$  and  $\tilde{\beta} \in [0, 1]$  (Boyko & Stone 2022), the 425 current result (3.28) applies to the limit of  $\tilde{\beta} \ll 1$ , while allowing De = O(1). 426

#### 3.2.1. Pressure drop at $O(\tilde{\beta})$ in the low-De limit 427

To calculate the pressure drop  $\Delta P_1$  at low Deborah numbers in the non-uniform shape region, 428 we use (3.13b)–(3.13c) and (3.27). The elastic normal stress (NS) contribution to the pressure 429 drop at  $O(\tilde{\beta})$  is 430

431 
$$\Delta P_{1}^{\text{NS}} = \frac{3}{2De} \int_{0}^{1} (1 - \eta^{2}) \left[ \tilde{A}_{11,0} \right]_{Z=1}^{Z=0} d\eta - \frac{3}{2De} \int_{0}^{1} \left[ \frac{H'(Z)}{H(Z)} \left( \int_{0}^{1} (1 - \eta^{2}) \tilde{A}_{11,0} d\eta \right) \right] dZ$$
  
432 
$$= \frac{27}{10} De(1 - H_{\ell}^{-4}) \quad \text{for} \quad De \ll 1, \quad (3.29)$$

where  $\begin{bmatrix} \tilde{A}_{11,0} \end{bmatrix}_{Z=1}^{Z=0} = \tilde{A}_{11,0}(0,\eta) - \tilde{A}_{11,0}(1,\eta).$ 433

The elastic shear stress (SS) contribution to the pressure drop at  $O(\tilde{\beta})$  is 434

435 
$$\Delta P_1^{\text{SS}} = -\frac{3}{De} \int_0^1 \left[ \frac{1}{H(Z)} \int_0^1 \eta \tilde{A}_{12,0} d\eta \right] dZ$$

436 
$$= 3 \int_0^1 \frac{\mathrm{d}Z}{H(Z)^3} + \frac{18}{10} De(1 - H_\ell^{-4}) \quad \text{for} \quad De \ll 1.$$
(3.30)

Substituting (3.29) and (3.30) into (3.27) provides the pressure drop at  $O(\tilde{\beta})$  in the low-*De* 437 limit up to O(De), 438

439 
$$\Delta P_1 = \frac{9}{2} De(1 - H_\ell^{-4}) + O(De^2) \quad \text{for} \quad De \ll 1, \tag{3.31}$$

so that the total pressure drop across the non-uniform channel in the low-De limit, accounting 440

441 for the leading-order effect of viscoelasticity, is

442 
$$\Delta P = \underbrace{3(1-\tilde{\beta})\int_{0}^{1}\frac{dZ}{H(Z)^{3}}}_{\text{Solvent stress}} + \underbrace{3\tilde{\beta}\int_{0}^{1}\frac{dZ}{H(Z)^{3}} + \frac{18}{10}\tilde{\beta}De(1-H_{\ell}^{-4})}_{\text{Elastic shear stress}} + \underbrace{\frac{27}{10}\tilde{\beta}De(1-H_{\ell}^{-4})}_{\text{Elastic normal stress}}$$
443 
$$= 3\int_{0}^{1}\frac{dZ}{H(Z)^{3}} + \frac{9}{2}\tilde{\beta}De(1-H_{\ell}^{-4}) + O(De^{2}) \quad \text{for} \quad De \ll 1, \quad (3.32)$$

in agreement with the results of our previous work (Boyko & Stone 2022). The three terms on

the right-hand side of (3.32) represent, respectively, the Newtonian solvent stress contribution, the elastic shear stress contribution, and the elastic normal stress contribution to the pressure

447 drop.

14

# 448 3.2.2. Pressure drop at $O(\tilde{\beta})$ in the high-De limit

To calculate the pressure drop  $\Delta P_1$  at high Deborah numbers in the non-uniform region, we use (3.17), (3.19), and (3.27). The elastic normal and shear stress contributions to the pressure drop at  $O(\tilde{\beta})$  are

$$\Delta P_1^{\rm NS} = \frac{9}{5} De(1 - H_\ell^{-2}) \quad \text{and} \quad \Delta P_1^{\rm SS} = 3 \int_0^1 \frac{dZ}{H(Z)} \quad \text{for} \quad De \gg 1. \quad (3.33a, b)$$

449 Substituting (3.33) into (3.27) yields the pressure drop at  $O(\tilde{\beta})$  in the high-*De* limit,

450 
$$\Delta P_1 = -3 \int_0^1 \frac{dZ}{H(Z)^3} + 3 \int_0^1 \frac{dZ}{H(Z)} + \frac{9}{5} De(1 - H_\ell^{-2}) \quad \text{for} \quad De \gg 1, \qquad (3.34)$$

so that the total pressure drop across the non-uniform channel in the high-De limit is

452 
$$\Delta P = \underbrace{3(1-\tilde{\beta})\int_{0}^{1}\frac{dZ}{H(Z)^{3}}}_{\text{Solvent stress}} + \underbrace{3\tilde{\beta}\int_{0}^{1}\frac{dZ}{H(Z)}}_{\text{Elastic shear stress}} + \underbrace{\frac{9}{5}\tilde{\beta}De(1-H_{\ell}^{-2})}_{\text{Elastic normal stress}} \quad \text{for} \quad De \gg 1. \quad (3.35)$$

Similar to the low-De limit, for the contraction geometry, the last term, corresponding to the 453 elastic normal stress contribution, leads to a decrease in the pressure drop, which is linear in 454 the Deborah number. As noted by Hinch et al. (2023), the tension in the streamlines at the end 455 of the contraction pulls the flow through the contraction, thus requiring less pressure to push. 456 Furthermore, at high Deborah numbers, the elastic shear stresses are lower than the fully 457 relaxed value  $\tilde{A}_{12} = -3De\eta/H_{\ell}^2$  due to insufficient time (distance) to approach their fully relaxed value in the contraction. Thus, the elastic shear stress contribution to the pressure 458 459 drop,  $3\tilde{\beta} \int_0^1 H(Z)^{-1} dZ$ , is smaller than the steady Poiseuille value of  $3\tilde{\beta} \int_0^1 H(Z)^{-3} dZ$ , so further reducing the pressure drop. Finally, we note that the result (3.35) also holds for the 460 461 expansion geometry  $H_{\ell} > 1$ , in which the two physical mechanisms mentioned above lead 462 to an increase in the pressure drop. 463

# 464 **4.** Low- $\tilde{\beta}$ lubrication analysis in the exit channel

In this section, we analyze the spatial relaxation of the elastic stresses and the pressure drop in the uniform exit channel. From examining the expressions (3.8)–(3.10) for the conformation tensor, when there are no longer shape changes, we expect the elastic stresses and the pressure in the exit channel to relax exponentially, with a strong dependence on  $De^{-1}$ . Thus, for higher Deborah numbers, a longer downstream section is required (Keiller 1993) for

	Contracting channel	Exit channel
<b>Deformation of the microstructure:</b>		
Semi-analytical solution	(3.8) - (3.10)	(B 3) - (B 5)
Low-De asymptotic solution	(3.13)	( <b>B</b> 7)
High-De asymptotic solution	(3.15), (3.17), (3.19)	( <b>B</b> 9)
Pressure drop:		
Semi-analytical solution	(3.28)	(4.1)
Low-De asymptotic solution	(3.32)	(4.3)
High-De asymptotic solution	(3.35)	(4.4)

TABLE 1. A summary of the semi-analytical solutions and low- and high-De asymptotic expressions for the deformation of the microstructure and the pressure drop of the Oldroyd-B fluid in a contraction and exit channel in the ultra-dilute limit.

polymer relaxation, consistent with previous numerical simulations using the Oldroyd-B 470 model (Debbaut et al. 1988; Alves et al. 2003). 471

Following similar steps as in the previous section, in appendix B, we derive closed-form 472 expressions for the conformation tensor and the pressure drop in the uniform exit channel for 473 arbitrary values of the Deborah number. Furthermore, we provide analytical expressions for 474 the conformation tensor and the pressure drop in the low- and high-De limits. We summarize 475 in table 1 the semi-analytical solutions and low- and high-De asymptotic expressions for 476 the deformation of the microstructure and the pressure drop of the Oldroyd-B fluid in a 477 contraction and exit channel in the ultra-dilute limit derived in this work. 478

In particular, we show that the total pressure drop in the exit channel can be expressed as 479

$$\Delta P_{\ell} = \underbrace{(1-\tilde{\beta})\frac{3L}{H_{\ell}^{3}}}_{\text{Solvent stress}} + \underbrace{\frac{3\tilde{\beta}}{2De}\int_{0}^{1}(1-\eta^{2})\left[\tilde{A}_{11,0}\right]_{Z_{\ell}=L}^{Z_{\ell}=0}d\eta}_{\text{Elastic normal stress}} + \underbrace{\frac{3\tilde{\beta}}{DeH_{\ell}}\int_{0}^{1}\eta\left[\int_{L}^{0}\tilde{A}_{12,0}dZ_{\ell}\right]d\eta}_{\text{Elastic shear stress}},$$

480

where  $L = \ell_{\ell}/\ell$  is the dimensionless length,  $H_{\ell} = H(Z = 1) = h_{\ell}/h_0$  is the dimensionless 481 height of the exit channel,  $Z_{\ell} = Z - 1$ ,  $\tilde{A}_{11,0}$  and  $\tilde{A}_{12,0}$  are given in (B4) and (B5), and 482  $\left[\tilde{A}_{11,0}\right]_{Z_{\ell}=L}^{Z_{\ell}=0} = \tilde{A}_{11,0}(Z_{\ell}=0,\eta) - \tilde{A}_{11,0}(Z_{\ell}=L,\eta).$ 483

It should be noted that we can express the first-order contribution  $\Delta P_{\ell,1}$  in terms of the 484 difference between the conformation tensor components at the beginning and end of the exit 485 channel (see appendix B and Hinch et al. (2023)), 486

$$487 \qquad \Delta P_{\ell,1} = \frac{3}{2De} \int_0^1 (1-\eta^2) \left[ \tilde{A}_{11,0} \right]_{Z_\ell=L}^{Z_\ell=0} d\eta - \frac{9}{2H_\ell^2} \int_0^1 \eta (1-\eta^2) \left[ \tilde{A}_{12,0} \right]_{Z_\ell=L}^{Z_\ell=0} d\eta \\
 + \frac{27De}{2H_\ell^4} \int_0^1 \eta^2 (1-\eta^2) \left[ \tilde{A}_{22,0} \right]_{Z_\ell=L}^{Z_\ell=0} d\eta. 
 \tag{4.2}$$

488

Hereafter, we assume that the length of the exit channel, L, is such that the elastic stresses reach 489 their fully relaxed values by the end of the exit channel, given by (2.16) with  $H \equiv H_{\ell}$ . Under 490 this assumption, (4.2) clearly shows that the first-order contribution  $\Delta P_{\ell,1}$  is *independent* of L 491 since the steady-state values of  $\tilde{A}_{11,0}$ ,  $\tilde{A}_{12,0}$ , and  $\tilde{A}_{22,0}$  depend solely on the  $\eta$  coordinate. Note, 492 however, that the total pressure in the exit channel depends on L via  $\Delta P_{\ell} = 3L/H_{\ell}^3 + \tilde{\beta}\Delta P_{\ell,1}$ . 493 In addition, we show in appendix B that the total pressure drop in the exit channel in the 494

(4.1)

(4.2)

495 low- and high-De limits are

$$\Delta P_{\ell} = \frac{3L}{H_{\ell}^3} - \frac{1728\tilde{\beta}De^3H''(1)}{35H_{\ell}^7} \quad \text{for} \quad De \ll 1,$$
(4.3)

$$\Delta P_{\ell} = \frac{3L}{H_{\ell}^3} + \frac{36}{5} \tilde{\beta} De(H_{\ell}^{-2} - H_{\ell}^{-4}) \quad \text{for} \quad De \gg 1.$$
(4.4)

From (4.3) and (4.4), it follows that, similar to the contraction, the pressure drop in the exit channel decreases with *De*. Furthermore, the physical mechanisms responsible for the pressure drop reduction are the same in both the contraction and the exit channels.

The asymptotic result (4.4) is obtained using expressions (B 9*a*)–(B 9*c*), which hold in the high-*De* limit within the core flow region. As discussed above, near the walls, there exists a viscoelastic boundary layer of thickness  $O(De^{-1})$ . Nevertheless, this boundary layer will contribute only a small  $O(\tilde{\beta}De^{-1})$  correction to the pressure drop in the exit channel for  $De \gg 1$ , as noted by Hinch *et al.* (2023).

# 507 **5. Results**

In this section, we present the theoretical results for the pressure drop and conformation tensor distribution of the Oldroyd-B fluid in the ultra-dilute limit developed in §§ 3 and 4.

510 As an illustrative example, we specifically consider the case of a smooth contraction of the

511 form

512

$$H(Z) = 1 - (1 - H_{\ell})Z^{2}(2 - Z)^{2} \qquad 0 \le Z \le 1,$$
(5.1)

where  $H_{\ell} = H(1)/H(0) = h_{\ell}/h_0$  is the ratio of the exit to entry heights; for the contracting geometry we have  $H_{\ell} < 1$ . This contraction shape function is illustrated in figure 2 and satisfies H'(0) = H'''(0) = 0 and H'(1) = H'''(1) = 0.

In this work, we present the results for  $H_{\ell} = 0.5$  and  $\tilde{\beta} = 0.05$ . While the current study 516 focuses only on one contraction ratio, in our previous work, we considered four contraction 517 ratios, in which the elastic normal stresses vary by almost two decades (Hinch et al. 2023). 518 In addition, figure 8 of our previous paper shows a 0.1 % difference between c = 0.1 and 519 c = 0.05 for the pressure drop in the contraction at De = 0.8. Nevertheless, our current 520 analysis allows one to analyze slowly varying arbitrarily shaped channels provided  $\epsilon \ll 1$ 521 and  $\tilde{\beta} \ll 1$ . To obtain the semi-analytical solutions for given values of De and  $H_{\ell}$ , we first 522 523 used MATLAB's routine cumtrapz to find the conformation tensor components, given in (3.8)–(3.10) and (B 3)–(B 5), for a contraction and exit channel. Typical values of the grid 524 size were  $\Delta Z = 10^{-4}$  and  $\Delta \eta = 0.005$ . We then used MATLAB's routine trapz to calculate 525 the pressure drop, (3.28) and (4.1), for a contraction and exit channel, respectively. 526

## 527 5.1. Streamwise variation of elastic stresses in the contraction and exit channel

We present in figure 3 the streamwise variation of the leading-order elastic stresses, scaled 528 by their entry values, on  $\eta = 0.5$  in contraction and exit channels for De = 0.01 (a, d), 529 De = 0.1 (b, e), and De = 1 (c, f). As expected, for a small Deborah number of De = 0.01, 530 531 the elastic stresses achieve their downstream fully relaxed values by the end of contraction (figure 3(a)), and thus we observe very little variation in the relaxation along the exit channel 532 (figure 3(d)). Consistent with the low-*De* asymptotic solutions (3.13), represented by cyan 533 dotted lines, for  $H_{\ell} = 0.5$ , the elastic shear and axial normal stresses increase by a factor of 534 4 and 16, respectively, while the transverse normal stress preserves its entry value. 535

For the case of De = 0.1, shown in figure 3(b, e), the elastic stresses do not have enough residence time to attain their downstream steady-state values in the contraction. Therefore,

16

Flow of an Oldroyd-B fluid in a slowly varying contraction



FIGURE 3. The streamwise variation of leading-order elastic stresses on  $\eta = 0.5$  in a smooth contraction and exit channel in the ultra-dilute limit. (a-c) Scaled elastic stresses  $\tilde{A}_{11,0}/(18De^2\eta^2)$ ,  $\tilde{A}_{12,0}/(-3De\eta)$ , and  $\tilde{A}_{22,0}$  in the contraction as a function of Z for (a) De = 0.01, (b) De = 0.1, and (c) De = 1. (d-e)Scaled elastic stresses in the exit channel  $\tilde{A}_{11,0}/(18De^2\eta^2)$ ,  $\tilde{A}_{12,0}/(-3De\eta)$ , and  $\tilde{A}_{22,0}$  as a function of  $Z_{\ell}$  for (d) De = 0.01, (e) De = 0.1, and (f) De = 1. Solid lines represent the semi-analytical solutions (3.8)–(3.10) (contraction) and (B 3)–(B 5) (exit channel). Cyan dotted lines represent the low-De asymptotic solutions (3.13) (contraction) and (B 7) (exit channel). Red dashed lines represent the high-De asymptotic solutions (3.15), (3.17), and (3.19) (contraction) and (B 9) (exit channel). All calculations were performed using  $H_{\ell} = 0.5$ .

there is a significant spatial relaxation in the exit channel. Interestingly, although the relaxation in the exit channel is governed mainly by  $e^{-2H_\ell Z_\ell/[3De(1-\eta^2)]}$  (see (B 3)–(B 5)), the elastic stresses relax over *slightly* different length scales, with the shortest relaxation distance required for  $\tilde{A}_{22,0}$  and the longest for  $\tilde{A}_{11,0}$ . The latter behavior is associated with the nature of the coupling between the elastic stresses so that  $\tilde{A}_{11,0}$  depends both on  $\tilde{A}_{12,0}$  on  $\tilde{A}_{22,0}$ , while  $\tilde{A}_{12,0}$  depends only on  $\tilde{A}_{22,0}$  (see (B 3)–(B 5)).

When De = 1, it is evident from figure 3(c) that, at the end of the contraction, the axial 544 normal stress increases by a factor of  $1/H_{\ell}^2 = 4$ , the transverse normal stress is squashed by a 545 factor of  $H_{\ell}^2 = 1/4$ , and the elastic shear stress preserves its entry value. Figure 3(f) presents 546 the spatial relaxation of the elastic stresses in the exit channel for De = 1, clearly showing 547 that a very long exit channel is required to attain the downstream fully relaxed values of 548 all stresses (L > 16 for  $\eta = 0.5$ ). Furthermore, we observe excellent agreement between 549 the semi-analytical results (solid lines) and the high-De asymptotic solutions (3.15), (3.17), 550 (3.19), and (B 9) (dashed red lines). Such an agreement for De = 1 is consistent with recent 551 results of Hinch *et al.* (2023), who found that the high-*De* analysis works well for De > 0.4. 552 The closed-form solutions for the conformation tensor components,  $(B_3)-(B_5)$ , clearly 553 554 show that the spatial relaxation of the elastic stresses in the exit channel strongly depends on the stresses at the end of the contraction (Z = 1). Therefore, it is of particular interest to 555



FIGURE 4. The cross-stream variation of leading-order elastic shear and normal stresses at the end of the contraction in the ultra-dilute limit. (a, c) Scaled elastic shear and normal stresses at the end of the contraction,  $(a) \tilde{A}_{12,0}(Z = 1, \eta)/(-3De\eta/H_{\ell}^2)$  and  $(c) \tilde{A}_{11,0}(Z = 1, \eta)/(18De^2\eta^2/H_{\ell}^4)$ , as a function of  $\eta$  for De = 0.01, 0.1, 1, and 10, respectively. (b)  $\tilde{A}_{12,0}(Z = 1, \eta)/(-3De\eta/H_{\ell}^2)$  and  $(d) \tilde{A}_{11,0}(Z = 1, \eta)/(18De^2\eta^2/H_{\ell}^4)$  as a function of the rescaled coordinate  $\zeta = De(1-\eta)$  for De = 0.1, 1, and 10. Solid lines represent the semi-analytical solutions (3.9)–(3.10). Cyan dotted lines represent the low-*De* asymptotic solutions (3.13*b*)–(3.13*c*). Red dashed lines represent the high-*De* asymptotic solutions (3.17) and (3.19). Green dashed lines represent the boundary-layer solutions (3.24*b*)–(3.24*c*). All calculations were performed using  $H_{\ell} = 0.5$ .

elucidate the behavior of the elastic stresses at the end of the contraction and the extent to which they are perturbed relative to their downstream fully relaxed values.

The solid lines in figure 4(a, c) present the elastic shear (a) and axial normal stresses 558 (c) at the end of the contraction as a function of  $\eta = y/H_{\ell}$  for De = 0.01, 0.1, 1, and 10, 559 scaled by their downstream fully relaxed values. For a small Deborah number of De = 0.01, 560  $\tilde{A}_{12,0}(Z=1,\eta)/(-3De\eta/H_{\ell}^2)$  and  $\tilde{A}_{11,0}(Z=1,\eta)/(18De^2\eta^2/H_{\ell}^4)$  only slightly differ from 561 their downstream values, and this behavior is well captured by the low-De asymptotic 562 solutions (3.13b)-(3.13c), represented by cyan dotted lines. As De increases, the elastic 563 564 stresses become considerably suppressed within the core flow region relative to their eventual relaxed values far downstream, and for De = 1 and De = 10, the elastic shear and axial 565 normal stresses approach the high-De asymptote of  $H_{\ell}^2 = 1/4$ , represented by red dashed 566 lines. Furthermore, in the high-De limit, we observe the presence of a viscoelastic boundary 567 layer close to the walls, where the elastic stresses reach their downstream fully relaxed values. 568 To provide insight into this viscoelastic boundary layer, we replot in figure 4(b, d) the 569 elastic shear (b) and axial normal stresses (d) at the end of the contraction as a function of

elastic shear (*b*) and axial normal stresses (*d*) at the end of the contraction as a function of the rescaled coordinate  $\zeta = De(1 - \eta)$  for De = 0.1, 1, and 10 (see § 3.1.3). It is evident from figures 4(*b*) and 4(*d*) that this rescaling collapses the results for the different Deborah numbers onto the same curves, which are the boundary-layer asymptotic solutions (3.24*b*) and (3.24*c*) (green dashed lines). Clearly, for De = 1 and De = 10, which are graphically almost indistinguishable, there is excellent agreement between the semi-analytical results



FIGURE 5. (a, b) Scaled elastic shear and normal stresses at the end of the contraction, (a)  $\tilde{A}_{12,0}(Z = 1, \eta)/(-3De\eta/H_{\ell}^2)$  and (b)  $\tilde{A}_{11,0}(Z = 1, \eta)/(18De^2\eta^2/H_{\ell}^4)$  minis  $H_{\ell}^2$ , divided by the factor  $1 - H_{\ell}^2$ , as a function of  $DeU_0(Z = 1, \eta)$  for De = 0.5, 1 and  $H_{\ell} = 0.125$ , 0.25, and 0.5. This rescaling leads to an approximate collapse of the results on the single uniform curve for different Deborah numbers and contraction ratios.

and the boundary-layer asymptotic solutions, thus confirming the thickness of a boundary layer as  $O(De^{-1})$ .

Furthermore, examining (3.8)–(3.10), we infer that their right-hand side is not a function of *De* and  $\eta$  separately but depends on the product  $DeU_0(Z, \eta)$ . To test this prediction, we show in figure 5(*a*, *b*) the scaled elastic shear (*a*) and axial normal stresses (*b*) at the end of the contraction, (*a*)  $\tilde{A}_{12,0}(Z = 1, \eta)/(-3De\eta/H_{\ell}^2)$  and (*b*)  $\tilde{A}_{11,0}(Z = 1, \eta)/(18De^2\eta^2/H_{\ell}^4)$ minus  $H_{\ell}^2$ , divided by the factor  $1 - H_{\ell}^2$ , as a function of  $DeU_0(Z = 1, \eta)$  for De = 0.5, 1and  $H_{\ell} = 0.125, 0.25, 0.5$ . We observe that the results for two different values of *De* approximately collapse onto the same curve across three contraction ratios.

## 5.2. Pressure gradient relaxation in the exit channel

It follows from figure 3(d-f) in the previous subsection that as De increases, there is a significant relaxation of the elastic stresses in the exit channel, which occurs over a long distance. Specifically, the elastic stresses relax exponentially over a distance which is proportional to the centerline velocity  $(3/2H_\ell)$  multiplied by the Deborah number De (see (B 3)–(B 5)). For this reason, a longer downstream section is required at higher De.

In this subsection, we study the relaxation of the pressure gradient in the downstream section. Substituting  $H(Z) = H_{\ell}$  into (2.19) yields the pressure gradient in the exit channel

593 
$$\frac{\mathrm{d}P}{\mathrm{d}Z} = -\frac{3(1-\tilde{\beta})}{H_{\ell}^3} + \frac{3\tilde{\beta}}{2De} \int_0^1 (1-\eta^2) \frac{\partial \tilde{A}_{11,0}}{\partial Z} \mathrm{d}\eta + \frac{3\tilde{\beta}}{H_{\ell}De} \int_0^1 \eta \tilde{A}_{12,0} \mathrm{d}\eta + O(\tilde{\beta}^2).$$
(5.2)

Noting that in the exit channel  $U_0 = (3/2H_\ell)(1-\eta^2)$  and  $dU_0/d\eta = -(3/H_\ell)\eta$ , and using the expression for  $U_0\partial \tilde{A}_{11,0}/\partial Z$  from (B 2c), (5.2) can be written as

596 
$$\left(\frac{\mathrm{d}P}{\mathrm{d}Z} + \frac{3}{H_{\ell}^3}\right)\frac{1}{\tilde{\beta}} = \frac{3}{H_{\ell}^3} - \frac{H_{\ell}}{De^2}\int_0^1 \tilde{A}_{11,0}\mathrm{d}\eta - \frac{3}{H_{\ell}De}\int_0^1 \eta \tilde{A}_{12,0}\mathrm{d}\eta, \tag{5.3}$$

597 where the right-hand side is independent of  $\tilde{\beta}$ .

585

We present in figure 6(a) the relaxation of the scaled pressure gradient  $(dP/dZ + 3/H_{\ell}^3)/\tilde{\beta}$ as a function of the downstream distance  $Z_{\ell}$  for De = 0.02, 0.2, 1, and 2. Similar to elastic stresses, the scaled pressure gradient relaxes exponentially over the downstream distance, which significantly increases with De. Furthermore, we observe a good agreement between the low- and high-De asymptotic solutions (cyan dotted and red dashed lines) and the semi-analytical results (solid lines).



FIGURE 6. The spatial relaxation of the pressure gradient for the Oldroyd-B fluid in the uniform exit channel of a contraction in the ultra-dilute limit. (a) Scaled pressure gradient  $(dP/dZ + 3/H_{\ell}^3)/\tilde{\beta}$  as a function of the downstream distance  $Z_{\ell}$  for De = 0.02, 0.2, 1, and 2. (b) Scaled pressure gradient  $(dP/dZ + 3/H_{\ell}^3)/\tilde{\beta}$  as a function of the rescaled downstream distance  $2H_{\ell}Z_{\ell}/3De$  in the log–linear plot. Solid lines represent the semi-analytical solutions obtained from (5.3) using (B 3)–(B 5). Cyan dotted lines represent the low-De asymptotic solutions obtained from (5.3) using (B 7). Red dashed lines represent the high-De asymptotic solutions obtained from (5.3) using (B 9). The green dashed line is  $100e^{-2H_{\ell}Z_{\ell}/3De}$ . All calculations were performed using  $H_{\ell} = 0.5$ .

Recalling that the elastic stresses relax exponentially over a distance proportional to  $(3De/2H_{\ell})$ , we replot in figure 6(*b*) the scaled pressure gradient, (5.3), as a function of the rescaled downstream distance  $2H_{\ell}Z_{\ell}/3De$  in the log–linear plot. As a result, all curves become parallel to the green dashed line  $100e^{-2H_{\ell}Z_{\ell}/3De}$ , thus confirming that the pressure gradient relaxes over a length scale  $\sim (3De/2H_{\ell})$ , similar to the elastic stresses. More specifically, it follows from figure 6(*b*) that the downstream distance over which the scaled pressure gradient (PG) decays to 1 % of its maximum value,  $L_{1\%}^{PG}$ , is approximately

611 
$$L_{1\%}^{PG} \approx (5.3 \pm 0.5) \times \frac{3De}{2H_{\ell}},$$
 (5.4)

where we obtain that the prefactor  $5.3 \pm 0.5$  is weakly dependent on *De* throughout the investigated range of Deborah numbers. Equation (5.4) and the scaling  $3De/2H_{\ell}$  indicate that in the exit channel, the appropriate Deborah number is based on the exit height, i.e.,  $De_{\text{exit}} = \lambda q/2h_{\ell}\ell = De/H_{\ell}$ .

We note that our estimate of the length of the downstream section, (5.4), is consistent with previous numerical studies on the viscoelastic flows in 2-D abrupt contractions (Debbaut *et al.* 1988; Alves *et al.* 2003). Specifically, (5.4) predicts  $L_{1\%}^{PG} \approx 239 \pm 23$  for  $De_{exit} = De/H_{\ell} = 30$ , which should be contrasted with 250 of Debbaut *et al.* (1988), who studied numerically the flow through the planar 4:1 contraction.

# 621 5.3. Pressure drop in the contraction and exit channel

In this subsection, we study the pressure drop across the contraction and the exit channel. 622 First, in figure 7(a) we present the non-dimensional pressure drop  $\Delta P = \Delta p / (\mu_0 q \ell / 2h_0^3)$ 623 in the contraction as a function of  $De = \lambda q/(2\ell h_0)$  for  $H_\ell = 0.5$  and  $\tilde{\beta} = 0.05$ . For further clarification, figure 7(b) shows the first-order contribution  $\Delta P_1 = \Delta p_1/(\mu_0 q \ell/2h_0^3)$ 624 625 as a function of  $De = \lambda q/(2\ell h_0)$ , which is independent of  $\tilde{\beta}$ . Black dots represent the 626 semi-analytical solution (3.28), cyan dotted lines represent the low-*De* asymptotic solution 627 (3.32), and red dashed lines represent the high-*De* asymptotic solution (3.35). Clearly, there 628 is excellent agreement between our low- and high-De asymptotic solutions and the semi-629 630 analytical results. We also validate the predictions of our semi-analytical and asymptotic results against the 2-D finite-element simulations with  $H_{\ell} = 0.5$ ,  $\tilde{\beta} = 0.05$ , and  $\epsilon = 0.02$ 631



FIGURE 7. Non-dimensional pressure drop for the Oldroyd-B fluid in a contracting channel in the ultra-dilute limit. (*a*) Dimensionless pressure drop  $\Delta P = \Delta p / (\mu_0 q \ell / 2h_0^3)$  as a function of  $De = \lambda q / (2\ell h_0)$  for  $\tilde{\beta} = 0.05$ . (*b*) First-order contribution  $\Delta P_1 = \Delta p_1 / (\mu_0 q \ell / 2h_0^3)$  to the dimensionless pressure drop as a function of  $De = \lambda q / (2\ell h_0)$ . Gray triangles in (*a*) represent the results of the finite-element simulation. Black dots represent the semi-analytical solution (3.28). Cyan dotted lines represent the low-*De* asymptotic solution (3.32). Red dashed lines represent the high-*De* asymptotic solution (3.35). All calculations were performed using  $H_{\ell} = 0.5$ .

(gray triangles), showing very good agreement. The details of the numerical implementation
 in the finite-element software COMSOL Multiphysics are provided in Boyko & Stone (2022).

It is evident that the semi-analytical solution for the pressure drop in the contraction 634 approaches the high-De asymptotic solution for  $De \gtrsim 0.4$  and linearly decreases with the 635 Deborah number. First, such an agreement for  $De \gg 1$  is consistent with our results for the 636 elastic stresses, shown in figure 3, and recent results of Hinch et al. (2023). Second, and 637 more importantly, from the excellent agreement between the semi-analytical results and the 638 high-De asymptotic solution, based on the components of the conformation tensor within 639 640 the core flow region, we conclude that the viscoelastic boundary layer near the walls makes a negligible contribution to the pressure drop in the contracting channel. 641

Next, in figure 8(a) we present the non-dimensional pressure drop  $\Delta P_{\ell}$  in the exit channel 642 as a function of De for  $H_{\ell} = 0.5$ ,  $\tilde{\beta} = 0.05$ , and L = 50. For De = 2, a long exit channel of 643  $L \gtrsim 30$  is required to reach the full relaxation of the elastic stresses and pressure gradient, 644 consistent with (5.4). Figure 8(b) shows the first-order contribution  $\Delta P_{\ell,1}$  as a function of 645 De, which is independent of  $\tilde{\beta}$ . In contrast to the total pressure drop  $\Delta P_{\ell}$ , the first-order 646 contribution  $\Delta P_{\ell,1}$  does not depend on L, as shown in (4.2), provided that L is sufficiently 647 long so that by the end of the exit channel the elastic stresses have achieved their fully relaxed 648 values (2.16) with  $H \equiv H_{\ell}$ . 649

The inset in figure 8(*a*) shows a comparison of our semi-analytical predictions (black dots) and finite-element simulation results (gray triangles) for  $\Delta P_{\ell} - \Delta P_{\ell,0} = \tilde{\beta} \Delta P_{\ell,1}$  as a function of *De* for  $H_{\ell} = 0.5$ ,  $\tilde{\beta} = 0.05$ , and L = 5. We observe excellent agreement between the semi-analytical and numerical results. In addition, the low-*De* asymptotic solution (cyan dotted curve) accurately captures the numerical results for De < 0.05 and indicates that the pressure drop in the exit channel scales as  $De^3$  for  $De \ll 1$ .

Similar to the contraction, the pressure drop in the exit channel linearly decreases with De 656 for  $De \ge 0.3$ , as shown in figure 8. While our semi-analytical solution linearly diminishes 657 with the slope of -36/5, as predicted by the high-*De* asymptotic solution (red dashed lines), 658 there is an offset between the two results for  $\tilde{\beta}\Delta P_{\ell,1}$ . In particular, for De = 0.4, we have 659 a non-negligible relative error of approximately 30 %. However, the inset in figure 8(b)660 shows that as De increases, the agreement between our semi-analytical solution and the 661 high-De asymptotic prediction significantly improves, resulting in relative errors of only 662 approximately 5 % and 1 % for De = 2 and De = 10, respectively. 663



FIGURE 8. Non-dimensional pressure drop for the Oldroyd-B fluid in the exit channel of a contraction in the ultra-dilute limit. (a) Dimensionless pressure drop  $\Delta P_{\ell} = \Delta p_{\ell}/(\mu_0 q \ell/2h_0^3)$  as a function of  $De = \lambda q/(2\ell h_0)$  for  $\tilde{\beta} = 0.05$  and L = 50. (b) First-order contribution  $\Delta P_{\ell,1} = \Delta p_{\ell,1}/(\mu_0 q \ell/2h_0^3)$  to the dimensionless pressure drop as a function of  $De = \lambda q/(2\ell h_0)$ . Black dots represent the semi-analytical solutions (4.1) ( $\Delta P_{\ell}$  in (a)) and (4.2) ( $\Delta P_{\ell,1}$  in (b)). The cyan dotted curve represents the low-Deasymptotic solution (4.3). Red dashed lines represent the high-De asymptotic solution (4.4). The inset in (a): a comparison of semi-analytical predictions (black dots) and finite-element simulation results (gray triangles) for  $\Delta P_{\ell} - \Delta P_{\ell,0} = \tilde{\beta} \Delta P_{\ell,1}$  as a function of De for  $\tilde{\beta} = 0.05$  and L = 5. The inset in (b):  $\Delta P_{\ell} - \Delta P_{\ell,0} = \tilde{\beta} \Delta P_{\ell,1}$  as a function of De for  $\tilde{\beta} = 0.05$  and L = 5. All calculations were performed using  $H_{\ell} = 0.5$ .

We note that our theoretical approach, based on the ultra-dilute limit, allows us to study the behavior of the elastic stresses and pressure drop at arbitrary values of De. In particular, we can predict the behavior in the high-Deborah-number regime, for example, De = 2 and even De = 10, which we are currently unable to access via finite-element simulations. Note, however, that we have assumed steady flows, so further investigation would be required to assess whether there might be flow instabilities at higher De.

## 670 5.4. Different contributions to the pressure drop in the contraction and exit channel

In the previous subsection, we observed a monotonic reduction in the dimensionless pressure drop with increasing De for an Oldroyd-B fluid flowing through the contraction and exit channel (figures 7 and 8). To understand the source of such pressure drop reduction, we elucidate the relative importance of elastic contributions to the pressure drop.

The elastic contributions to the non-dimensional pressure drop across the contraction and 675 exit channel, scaled by  $\hat{\beta}$ , as a function of *De* are shown in figures 9(a) and 9(b), respectively. 676 Black circles and gray dots represent the elastic shear and normal stress contributions obtained 677 from the semi-analytical solutions (3.28) and (4.1). Cyan dotted and purple curves represent 678 the elastic shear and normal stress contributions obtained from the low-De asymptotic 679 680 solutions (3.32) and (4.3). Red and black dashed lines represent the elastic shear and normal stress contributions obtained from the high-De asymptotic solutions (3.35) and (4.4). As 681 expected based on our previous results, we observe excellent agreement between our low-682 and high-De asymptotic solutions and the semi-analytical predictions. 683

The first main source for the pressure drop reduction is the elastic normal stress contribution, which linearly decreases with *De* in the contraction and exit channel at low and high Deborah numbers. As noted by Hinch *et al.* (2023), this is because the elastic normal stresses, which correspond to the tension in the streamlines, are higher at the end of the contraction (exit channel) compared with the beginning of the contraction (exit channel). These higher elastic normal stresses pull the fluid along and thus require less pressure to push.

The second main source for the pressure drop reduction is the decrease of elastic shear stress contribution with De due to the long time (or long distance) required for the elastic shear stresses to approach their eventual relaxed values far downstream. As a result, the



FIGURE 9. Elastic contributions to the non-dimensional pressure drop of the Oldroyd-B fluid, scaled by  $\tilde{\beta}$ , in (*a*) the contraction and (*b*) the exit channel in the ultra-dilute limit. Black circles and gray dots represent the semi-analytical solutions (3.28) (contraction) and (4.1) (exit channel) for elastic shear and normal stress contributions. Cyan dotted and purple curves represent the low-*De* asymptotic solutions (3.32) (contraction) and (4.3) (exit channel) for elastic shear and normal stress contributions. Red and black dashed lines represent the high-*De* asymptotic solutions (3.35) (contraction) and (4.4) (exit channel) for elastic shear and normal stress contributions. All calculations were performed using  $H_{\ell} = 0.5$  and L = 50.

elastic shear stresses are lower than the fully relaxed value  $\tilde{A}_{12} = -3De\eta/H_{\ell}^2$  (see figure 3), and their contribution to the pressure drop is smaller than the steady Poiseuille value of  $3\tilde{\beta}\int_0^1 H(Z)^{-3}dZ$  (contraction) and  $3\tilde{\beta}L/H_{\ell}^3$  (exit channel), thus reducing the pressure drop. At low Deborah numbers, such a decrease scales as De and  $De^3$  for a smooth contraction and exit channel, respectively. However, at high Deborah numbers, it approaches a constant asymptotic value of  $3\tilde{\beta}\int_0^1 H(Z)^{-1}dZ$  for the contraction. For the exit channel,  $\Delta P_{\ell,1}^{SS}$  linearly depends on the Deborah number since the relaxation of the elastic shear stresses occurs over the distance L, which scales linearly with De, as shown in (5.4).

# 701 6. Concluding remarks

In this work, we applied the lubrication approximation and considered the ultra-dilute 702 limit to study the flow of an Oldroyd-B fluid in arbitrarily shaped contracting channels. 703 704 Specifically, we exploited the one-way coupling between the parabolic velocity and polymer conformation tensor in the ultra-dilute limit to derive closed-form expressions for the 705 microstructure deformation and the flow rate-pressure drop relation for arbitrary values 706 of the Deborah number. We provided analytical expressions for the conformation tensor 707 and the  $q - \Delta p$  relation in the low- and high Deborah limits for the contraction and exit 708 channels, complementing the asymptotic results of Boyko & Stone (2022) and the analysis 709 of Hinch et al. (2023) at any concentration. We further analyzed the viscoelastic boundary 710 layer of a thickness  $O(De^{-1})$ , existing near the walls at high Deborah numbers, and derived 711 the boundary-layer asymptotic solutions. We validated our semi-analytical and asymptotic 712 results for the pressure drop in the smooth contraction and exit channels with 2-D finite-713 element numerical simulations and found excellent agreement. 714

For both contraction and exit channels, the pressure drop of an Oldroyd-B fluid monotonically decreases with increasing De and scales linearly with De at high Deborah numbers, as shown in figures 7 and 8. We identified two mechanisms for such pressure drop reduction (see figure 9). The first is higher elastic normal stresses at the end of the contraction and exit channels, relative to the corresponding entry values, that pull the fluid along and thus require less pressure to push. The second source for the pressure drop reduction is because, once perturbed from their upstream values, the elastic shear stresses require a long distance to approach their new downstream fully relaxed values, as shown in figure 3, so again reducingthe pressure drop.

Our theoretical approach, which relies on lubrication theory and the ultra-dilute limit, 724 allows us to study the behavior of the elastic stresses and pressure drop of an Oldroyd-B 725 fluid at arbitrary values of *De*. Our theory is not restricted to the case of two-dimensional 726 contracting channels and can be utilized to study different slowly varying geometries, such as 727 728 expansions and constrictions. The approach can also be extended to axisymmetric geometries. Furthermore, the theoretical framework we presented enables us to access sufficiently high 729 Deborah numbers, which are difficult and sometimes impossible to study via numerical 730 simulations due to the high-Weissenberg-number problem (Owens & Phillips 2002; Alves 731 et al. 2021). We, therefore, believe that our analytical and semi-analytical results for the 732 733 ultra-dilute limit are of fundamental importance as they may serve for simulation validation. Finally, we note that our theoretical predictions for the pressure drop reduction of an 734 735 Oldroyd-B fluid in a contraction are consistent with the previous numerical reports on 2-D abruptly contracting geometries (Aboubacar et al. 2002; Alves et al. 2003; Binding et al. 2006; 736 737 Aguayo et al. 2008). However, these predictions are opposite to the experiments showing a nonlinear increase in the pressure drop with *De* for the flow of a Boger fluid through abrupt 738 axisymmetric contraction-expansion and contraction geometries (Rothstein & McKinley 739 1999, 2001; Nigen & Walters 2002; Sousa et al. 2009). As noted by Alves et al. (2003) and 740 Hinch et al. (2023), this discrepancy might be attributed to the lack of dissipative effects 741 in the Oldroyd-B model. Thus, as a future research direction, it is interesting to study more 742 complex constitutive equations, such as a finitely extensible nonlinear elastic (FENE) model 743 introduced by Chilcott & Rallison (1988) (FENE-CR) and a finitely extensible nonlinear 744 elastic model with the Peterlin approximation (FENE-P), that incorporate dissipation and 745 additional microscopic features of polymer solutions and understand how these features 746 affect the pressure drop. We anticipate that even for a more complex constitutive model, the 747 748 theoretical framework presented here will enable the development of a simplified, reducedorder theory, allowing us to study the behavior at non-small Deborah numbers. 749

750 Funding, E.B. acknowledges the support by grant no. 2022688 from the US-Israel Binational Science

Foundation (BSF). H.A.S. acknowledges the support from grant no. CBET-2246791 from the United States
 National Science Foundation (NSF).

753 Declaration of interests. The authors report no conflict of interest.

### 754 Author ORCIDs.

755 Evgeniy Boyko https://orcid.org/0000-0002-9202-5154;

756 John Hinch https://orcid.org/0000-0003-3130-7761;

757 Howard A. Stone https://orcid.org/0000-0002-9670-0639.

# 758 Appendix A. Orthogonal curvilinear coordinates for a slowly varying geometry

In this appendix we provide additional details for orthogonal curvilinear coordinates for a slowly varying geometry used in our theoretical analysis. We consider a slowly spatially varying channel with a given shape *h* that varies on the length scale  $\ell$ , so that  $h = h(z/\ell) =$  $h_0H(Z)$ . We transform the Cartesian coordinates (Z, Y) to curvilinear coordinates  $(\xi, \eta)$  with the mapping

$$\xi = Z + \epsilon^2 Q(Z, Y), \qquad \eta = \frac{Y}{H(Z)}, \tag{A1}$$

where  $Z = z/\ell$ ,  $Y = y/h_0$ , and Q is an unknown function yet to be determined. Note that, in the lubrication limit, the orthogonal coordinate  $\xi$  (scaled by  $\ell$ ) is nearly in the z-direction.

We find Q(Z, Y) by requiring that the curvilinear coordinates  $(\xi, \eta)$  are orthogonal, i.e.,

768  $\nabla \xi \cdot \nabla \eta = 0$ . Using the relations

769  
770
$$\boldsymbol{\nabla}\boldsymbol{\xi} = \left[\boldsymbol{\epsilon}\frac{\partial\boldsymbol{\xi}}{\partial\boldsymbol{Z}}, \frac{\partial\boldsymbol{\xi}}{\partial\boldsymbol{Y}}\right] = \left[\boldsymbol{\epsilon}\left(1 + \boldsymbol{\epsilon}^2\frac{\partial\boldsymbol{Q}}{\partial\boldsymbol{Z}}\right), \boldsymbol{\epsilon}^2\frac{\partial\boldsymbol{Q}}{\partial\boldsymbol{Y}}\right], \quad (A\,2a)$$

$$\boldsymbol{\nabla}\eta = \left[\epsilon \frac{\partial \eta}{\partial Z}, \frac{\partial \eta}{\partial Y}\right] = \left[-\epsilon \frac{YH'(Z)}{H(Z)^2}, \frac{1}{H(Z)}\right],\tag{A2b}$$

772 we obtain

771

788

795

799

773 
$$\boldsymbol{\nabla}\boldsymbol{\xi}\cdot\boldsymbol{\nabla}\boldsymbol{\eta} = \frac{\epsilon^2}{H(Z)} \left[ -\left(1 + \epsilon^2 \frac{\partial Q}{\partial Z}\right) \frac{YH'(Z)}{H(Z)} + \frac{\partial Q}{\partial Y} \right]. \tag{A3}$$

Therefore,  $\nabla \xi \cdot \nabla \eta = O(\epsilon^4)$  provided we set

775 
$$\frac{\partial Q}{\partial Y} = \frac{YH'(Z)}{H(Z)} \Rightarrow Q(Z,Y) = -\frac{1}{2}\frac{H'(Z)}{H(Z)}(H(Z)^2 - Y^2), \tag{A4}$$

where without loss of generality, we choose  $Q \equiv 0$  on Y = H(Z). Hence, the orthogonal curvilinear coordinates  $(\xi, \eta)$  are

778 
$$\xi = Z - \frac{1}{2}\epsilon^2 \frac{H'(Z)}{H(Z)} (H(Z)^2 - Y^2) + O(\epsilon^4), \qquad \eta = \frac{Y}{H(Z)}.$$
 (A 5)

<sup>779</sup> Using (A 5), the inverse transformation is (see also Hinch *et al.* 2023)

780 
$$Z = \xi + \frac{1}{2}\epsilon^2 H'(\xi)H(\xi)(1-\eta^2) + O(\epsilon^4) = \xi + \frac{1}{4}(H(\xi)^2)'(1-\eta^2) + O(\epsilon^4), \quad (A \, 6a)$$
781

782 
$$Y(\xi,\eta) = \eta H(\xi), \tag{A6b}$$

where evaluating  $H(\xi)$  rather than H(Z) introduces a relative error of  $O(\epsilon^2)$ .

In what follows, it is also convenient to use the dimensional form of the transformation (A 6), given as

786 
$$z = \bar{\xi} + \frac{1}{2}\epsilon h_0 \frac{dH(\xi)}{d\xi} H(\xi)(1-\eta^2) + O(\epsilon^4), \qquad y = \eta h_0 H(\xi),$$
(A7)

787 where we have defined the dimensional coordinate  $\bar{\xi} = \xi \ell$ .

The expressions for the curvilinear orthonormal basis vectors  $\mathbf{e}_{\xi}$  and  $\mathbf{e}_{\eta}$  in terms of  $\mathbf{e}_{z}$  and  $\mathbf{e}_{y}$  are obtained from

791 
$$\mathbf{e}_{\xi} = \frac{\partial \mathbf{x}}{\partial \bar{\xi}} \frac{1}{|\partial \mathbf{x}/\partial \bar{\xi}|}, \qquad \mathbf{e}_{\eta} = \frac{\partial \mathbf{x}}{\partial \eta} \frac{1}{|\partial \mathbf{x}/\partial \eta|}, \tag{A8}$$

792 where using (A7), we have

$$\begin{array}{l} 793 \\ 794 \end{array} \qquad \qquad \frac{\partial \boldsymbol{x}}{\partial \bar{\xi}} = \left(\frac{\partial z}{\partial \bar{\xi}}, \frac{\partial y}{\partial \bar{\xi}}\right) = \left(1 + O(\epsilon^2), h_0 \frac{\mathrm{d}H(\xi)}{\mathrm{d}\bar{\xi}}\eta\right) \underset{\bar{\xi} = \ell\,\xi}{=} \left(1 + O(\epsilon^2), \epsilon \frac{\mathrm{d}H(\xi)}{\mathrm{d}\xi}\eta\right), \qquad (A\,9a)$$

$$\frac{\partial \boldsymbol{x}}{\partial \eta} = \left(\frac{\partial z}{\partial \eta}, \frac{\partial y}{\partial \eta}\right) = \left(-\epsilon h_0 \frac{\mathrm{d}H(\xi)}{\mathrm{d}\xi} H(\xi)\eta, h_0 H(\xi)\right),\tag{A9b}$$

and  $h_{\xi} = \left| \partial \mathbf{x} / \partial \bar{\xi} \right| \approx 1$  and  $h_{\eta} = \left| \partial \mathbf{x} / \partial \eta \right| \approx h_0 H(\xi) = h(\bar{\xi}/\ell)$  are the metric coefficients (or scale factors) in the  $\xi$ - and  $\eta$ -directions, respectively, with small corrections of  $O(\epsilon^2)$ .

Substituting (A 9) into (A 8), we obtain

$$\mathbf{e}_{\xi} \approx \mathbf{e}_{z} + \epsilon H'(\xi) \eta \mathbf{e}_{y}, \qquad \mathbf{e}_{\eta} \approx -\epsilon H'(\xi) \eta \mathbf{e}_{z} + \mathbf{e}_{y}. \tag{A10}$$

## 800 A.2. Velocity and conformation tensor in Cartesian and curvilinear coordinates

The velocity field and the conformation tensor can be expressed either in Cartesian or curvilinear coordinates. Specifically, the velocity  $\mathbf{u} = u_z \mathbf{e}_z + u_y \mathbf{e}_y$  in Cartesian coordinates is related to the velocity  $\mathbf{u} = u \mathbf{e}_{\mathcal{E}} + v \mathbf{e}_n$  in curvilinear coordinates through (Brand 1947)

804 
$$\begin{pmatrix} u_z \\ u_y \end{pmatrix} = \boldsymbol{M} \cdot \begin{pmatrix} u \\ v \end{pmatrix}, \qquad (A \ 11)$$

where M is the coordinate transformation matrix obtained from (A 10) and given as

806 
$$\boldsymbol{M} = \begin{pmatrix} 1 & -\epsilon H'(\xi)\eta \\ \epsilon H'(\xi)\eta & 1 \end{pmatrix}.$$
 (A 12)

We introduce non-dimensional velocity components in curvilinear coordinates, similar to the non-dimensionalization (2.5a),

809 
$$U = \frac{u}{u_c}, \qquad V = \frac{v}{\epsilon u_c}.$$
 (A 13)

Using (A 11)–(A 13) provides the relations between non-dimensional velocity components in different coordinates

812 
$$U_z = U - \epsilon^2 \eta H'(\xi) V, \qquad U_y = \eta H'(\xi) U + V.$$
 (A 14)

813 While velocity in the *z*- and  $\xi$ -directions are the same, albeit to a  $O(\epsilon^2)$  correction, the 814 velocity in the *y*-direction is greater by  $\eta H'(\xi)U$  than the velocity in the  $\eta$ -direction.

Similarly, the conformation tensor  $\mathbf{A} = A_{zz}\mathbf{e}_{z}\mathbf{e}_{z} + A_{zy}(\mathbf{e}_{z}\mathbf{e}_{y} + \mathbf{e}_{y}\mathbf{e}_{z}) + A_{yy}\mathbf{e}_{y}\mathbf{e}_{y}$  in Cartesian coordinates is related to the conformation tensor  $\mathbf{A} = A_{11}\mathbf{e}_{\xi}\mathbf{e}_{\xi} + A_{12}(\mathbf{e}_{\xi}\mathbf{e}_{\eta} + \mathbf{e}_{\eta}\mathbf{e}_{\xi}) + A_{22}\mathbf{e}_{\eta}\mathbf{e}_{\eta}$ in curvilinear coordinates through (Brand 1947)

818 
$$\begin{pmatrix} A_{zz} & A_{zy} \\ A_{yz} & A_{yy} \end{pmatrix} = \boldsymbol{M} \cdot \begin{pmatrix} A_{11} & A_{12} \\ A_{21} & A_{22} \end{pmatrix} \cdot \boldsymbol{M}^{\mathrm{T}}.$$
 (A15)

Next, we define scaled  $\tilde{A}_{11}$ ,  $\tilde{A}_{12}$ , and  $\tilde{A}_{22}$  in curvilinear coordinates, similar to the nondimensionalization (2.5*c*),

821  $\tilde{A}_{11} = \epsilon^2 A_{11}, \qquad \tilde{A}_{12} = \epsilon A_{12}, \qquad \tilde{A}_{22} = A_{22}.$  (A 16)

Finally, using (A 12) and (A 15)–(A 16), we obtain the relations between conformation tensor components in different coordinates

824  
825 
$$\tilde{A}_{zz} = \tilde{A}_{11} + O(\epsilon^2),$$
 (A 17*a*)

$$\tilde{A}_{zy} = \tilde{A}_{12} + \eta H'(\xi) \tilde{A}_{11} + O(\epsilon^2), \qquad (A\,17b)$$

828 
$$\tilde{A}_{yy} = \tilde{A}_{22} + 2\eta H'(\xi) \tilde{A}_{12} + \eta^2 (H'(\xi))^2 \tilde{A}_{11} + O(\epsilon^2).$$
(A 17c)

# Appendix B. Low- $\tilde{\beta}$ lubrication analysis in the exit channel: detailed derivation

We here provide details of the derivation of closed-form expressions for the conformation tensor and the pressure drop in the uniform exit channel for  $\tilde{\beta} \ll 1$ .

B.1. Velocity, conformation, and pressure drop in the exit channel at the leading order in  $\tilde{\beta}$ The velocity field and pressure drop in the exit channel at the leading order in  $\tilde{\beta}$  are

$$U_0 = \frac{3}{2} \frac{1}{H_\ell} (1 - \eta^2), \qquad V_0 \equiv 0, \qquad \Delta P_{\ell,0} = \frac{3L}{H_\ell^3}. \tag{B1a-c}$$

Substituting  $(\underline{B} \ 1a)$  into (3.6), we obtain the governing equations for the conformation 836 tensor components in the exit channel at the leading order in  $\hat{\beta}$ , 837

838  
839  

$$U_0 \frac{\partial \tilde{A}_{22,0}}{\partial Z} = -\frac{1}{De} (\tilde{A}_{22,0} - 1),$$
 (B 2*a*)

840  
841  

$$U_0 \frac{\partial A_{12,0}}{\partial Z} - \frac{1}{H_\ell} \frac{dU_0}{d\eta} \tilde{A}_{22,0} = -\frac{1}{De} \tilde{A}_{12,0},$$
 (B 2b)

842 
$$U_0 \frac{\partial \tilde{A}_{11,0}}{\partial Z} - \frac{2}{H_\ell} \frac{dU_0}{dn} \tilde{A}_{12,0} = -\frac{1}{De} \tilde{A}_{11,0}.$$
(B 2c)

Equations (B 2), similar to (3.6), represent a set of one-way coupled first-order semi-linear 843 partial differential equations that can be solved first for  $\tilde{A}_{22,0}$ , followed by  $\tilde{A}_{12,0}$ , and then for 844  $\tilde{A}_{11,0}$ . The solution of these equations is 845

846 
$$\tilde{A}_{22,0} = 1 + (\tilde{A}_{22,0}^{\text{ref}}(\eta) - 1)e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]},$$
(B 3)  
847

848 
$$\tilde{A}_{12,0} = -\frac{3De}{H_{\ell}^2}\eta + e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]} \left[\tilde{A}_{12,0}^{\text{ref}}(\eta) + \frac{3De}{H_{\ell}^2}\eta - \frac{2\eta(\tilde{A}_{22,0}^{\text{ref}}(\eta) - 1)Z_{\ell}}{H_{\ell}(1-\eta^2)}\right], \quad (B 4)$$

850 
$$\tilde{A}_{11,0} = \frac{18De^2}{H_{\ell}^4} \eta^2 + e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]} \left[ \tilde{A}_{11,0}^{\text{ref}}(\eta) - \frac{18De^2}{H_{\ell}^4} \eta^2 \right]$$

851 
$$+\frac{4\eta^2 (\tilde{A}_{22,0}^{\text{ref}}(\eta) - 1)Z_{\ell}^2}{H_{\ell}^2 (1 - \eta^2)^2} - \frac{4\eta Z_{\ell} [3De\eta + H_{\ell}^2 \tilde{A}_{12,0}^{\text{ref}}(\eta)]}{H_{\ell}^3 (1 - \eta^2)} \bigg], \quad (B5)$$

where  $Z_{\ell} = Z - 1$  and  $\tilde{A}_{22,0}^{\text{ref}}(\eta) = \tilde{A}_{22,0}(Z = 1, \eta)$ ,  $\tilde{A}_{12,0}^{\text{ref}}(\eta) = \tilde{A}_{12,0}(Z = 1, \eta)$ , and  $\tilde{A}_{11,0}^{\text{ref}}(\eta) = \tilde{A}_{12,0}(Z = 1, \eta)$ . 852  $\tilde{A}_{11,0}(Z=1,\eta)$  are the reference distributions of the conformation tensor components at the 853

854 outlet (Z = 1) of the non-uniform channel that can be obtained from (3.8), (3.9), and (3.10). We note that under the assumption of a fully developed flow in the entire exit channel so that 855

 $U(\eta) = (3/2H_{\ell})(1-\eta^2)$ , the governing equations for the conformation tensor components 856 (B 2) and their solution (B 3)–(B 5) are valid not only at  $O(\tilde{\beta}^0)$  but for arbitrary values of  $\tilde{\beta}$ . 857 Finally, we note that the components of the conformation tensor at the walls of the exit 858 channel  $(\eta = \pm 1)$  are given in (3.12), with  $H(Z) \equiv H_{\ell}$ . Thus, the conformation tensor 859 components at the walls of the exit channel attain their fully relaxed values without spatial 860 development. 861

#### B.1.1. Conformation tensor in the exit channel at low De numbers 862

At low Deborah numbers, we use (3.13) to obtain the reference distributions of the 863 conformation tensor components at the beginning of the exit channel, 864

865 
$$\tilde{A}_{22,0}^{\text{ref}}(\eta) = 1 - \frac{9De^2 H''(1)}{2H_{\ell}^3} (1 - \eta^2)^2, \qquad (B \, 6a)$$

866

867 
$$\tilde{A}_{12,0}^{\text{ref}}(\eta) = -\frac{3De}{H_{\ell}^2}\eta + \frac{81De^3H''(1)}{2H_{\ell}^5}\eta(1-\eta^2)^2, \tag{B}6b$$

868

28

869 
$$\tilde{A}_{11,0}^{\text{ref}}(\eta) = \frac{18De^2}{H_{\ell}^4}\eta^2 - \frac{486De^4H^{\prime\prime}(1)}{H_{\ell}^7}\eta^2(1-\eta^2)^2, \qquad (B\,6c)$$

where for a smooth geometry, we have assumed that H'(1) = H'''(1) = 0. 870

Substituting (B 6) into (B 3), we obtain explicit expressions for the spatial relaxation of the 871 conformation tensor components in the exit channel for  $De \ll 1$ , 872

873 
$$\tilde{A}_{22,0} = 1 - \frac{9De^2H''(1)}{2H_{\ell}^3}(1-\eta^2)^2 e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]}, \qquad (B7a)$$

875 
$$\tilde{A}_{12,0} = -\frac{3De}{H_{\ell}^2}\eta + \frac{9De^2H''(1)}{H_{\ell}^4}\eta(1-\eta^2)e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]}\left[\frac{9De}{2H_{\ell}}(1-\eta^2) + Z_{\ell}\right], \text{ (B 7b)}$$
876

877 
$$\tilde{A}_{11,0} = \frac{18De^2}{H_{\ell}^4} \eta^2 - \frac{18De^2 H''(1)}{H_{\ell}^5} \eta^2 e^{-2H_{\ell} Z_{\ell} / [3De(1-\eta^2)]} \left[ \frac{27De^2}{H_{\ell}^2} (1-\eta^2)^2 \right]$$

$$+Z_{\ell}^{2} + \frac{9De}{H_{\ell}}Z_{\ell}(1-\eta^{2})\bigg].$$
 (B7c)

#### B.1.2. Conformation tensor in the exit channel at high De numbers 880

From (3.15), (3.17), and (3.19) it follows that the reference distributions of the conformation 881 tensor components at the beginning of the exit channel within the core flow region in the 882 high-De limit are 883

884 
$$\tilde{A}_{22,0}^{\text{ref}}(\eta) = H_{\ell}^2, \qquad \tilde{A}_{12,0}^{\text{ref}}(\eta) = -3De\eta, \qquad \tilde{A}_{11,0}^{\text{ref}}(\eta) = \frac{18De^2}{H_{\ell}^2}\eta^2.$$
 (B 8)

Substituting (B 8) into (B 3) provides expressions for the spatial relaxation of the conforma-885 tion tensor components in the exit channel for  $De \gg 1$ , 886

887  
888  

$$\tilde{A}_{22,0} = 1 + (H_{\ell}^2 - 1)e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]},$$
 (B 9*a*)

889 
$$\tilde{A}_{12,0} = -\frac{3De\eta}{H_{\ell}^2} + e^{-2H_{\ell}Z_{\ell}/[3De(1-\eta^2)]} \left[ -3De\eta + \frac{3De\eta}{H_{\ell}^2} + \frac{2\eta(1-H_{\ell}^2)Z_{\ell}}{H_{\ell}(1-\eta^2)} \right], \quad (B\,9b)$$

891 
$$\tilde{A}_{11,0} = \frac{18De^2\eta^2}{H_\ell^4} + e^{-2H_\ell Z_\ell / [3De(1-\eta^2)]} \left[ \frac{18De^2\eta^2}{H_\ell^2} - \frac{18De^2\eta^2}{H_\ell^4} \right]$$

892
$$+\frac{4\eta^2(H_{\ell}^2-1)Z_{\ell}^2}{H_{\ell}^2(1-\eta^2)^2}-\frac{12De\eta^2 Z_{\ell}(1-H_{\ell}^2)}{H_{\ell}^3(1-\eta^2)}\right].$$
(B9c)

893

894

# B.2. Pressure drop in the exit channel at the first order in $\tilde{\beta}$

Using (2.21) and (3.27), the expressions for the pressure drop at  $O(\tilde{\beta})$ ,  $\Delta P_{\ell,1}$ , and the total 895 pressure drop in the exit channel up to  $O(\tilde{\beta}), \Delta P_{\ell}$ , are 896

897 
$$\Delta P_{\ell,1} = -\frac{3L}{H_{\ell}^3} + \frac{3}{2De} \int_0^1 (1-\eta^2) \left[ \tilde{A}_{11,0} \right]_{Z_{\ell}=L}^{Z_{\ell}=0} d\eta + \frac{3}{DeH_{\ell}} \int_0^1 \eta \left[ \int_L^0 \tilde{A}_{12,0} dZ_{\ell} \right] d\eta, \quad (B\ 10)$$

898 and

$$\Delta P_{\ell} = \underbrace{(1 - \tilde{\beta})\frac{3L}{H_{\ell}^{3}}}_{\text{Solvent stress}} + \underbrace{\frac{3\tilde{\beta}}{2De}\int_{0}^{1}(1 - \eta^{2})\left[\tilde{A}_{11,0}\right]_{Z_{\ell}=L}^{Z_{\ell}=0}d\eta}_{\text{Elastic normal stress}} + \underbrace{\frac{3\tilde{\beta}}{DeH_{\ell}}\int_{0}^{1}\eta\left[\int_{L}^{0}\tilde{A}_{12,0}dZ_{\ell}\right]d\eta}_{\text{Elastic shear stress}},$$

899

where  $\tilde{A}_{11,0}$  and  $\tilde{A}_{12,0}$  are given in (B 4) and (B 5) and  $\begin{bmatrix} \tilde{A}_{11,0} \end{bmatrix}_{Z_{\ell}=L}^{Z_{\ell}=0} = \tilde{A}_{11,0}(Z_{\ell} = 0, \eta) - \tilde{A}_{11,0}(Z_{\ell} = L, \eta)$ . The three terms on the right-hand side of (B 11) represent, respectively, the Newtonian solvent stress contribution, the elastic normal stress contribution, and the elastic shear stress contribution to the pressure drop.

It is possible to express the first-order contribution  $\Delta P_{\ell,1}$  in terms of the difference between the conformation tensor components at the beginning and end of the exit channel. First, integrating (B 2*a*) and (B 2*b*) with respect to  $Z_{\ell}$  from *L* to 0, we obtain

907 
$$U_0 \left[ \tilde{A}_{22,0} \right]_{Z_\ell = L}^{Z_\ell = 0} = -\frac{1}{De} \int_L^0 (\tilde{A}_{22,0} - 1) dZ_\ell, \tag{B12}$$

908

909 
$$U_0 \left[ \tilde{A}_{12,0} \right]_{Z_\ell = L}^{Z_\ell = 0} - \frac{1}{H_\ell} \frac{\mathrm{d}U_0}{\mathrm{d}\eta} \int_L^0 \tilde{A}_{22,0} \mathrm{d}Z_\ell = -\frac{1}{De} \int_L^0 \tilde{A}_{12,0} \mathrm{d}Z_\ell. \tag{B13}$$

910 Substituting (B 12) into (B 13) yields

911 
$$U_0 \left[ \tilde{A}_{12,0} \right]_{Z_\ell = L}^{Z_\ell = 0} + \frac{De}{H_\ell} \frac{\mathrm{d}U_0}{\mathrm{d}\eta} U_0 \left[ \tilde{A}_{22,0} \right]_{Z_\ell = L}^{Z_\ell = 0} + \frac{L}{H_\ell} \frac{\mathrm{d}U_0}{\mathrm{d}\eta} = -\frac{1}{De} \int_L^0 \tilde{A}_{12,0} \mathrm{d}Z_\ell.$$
(B 14)

912 Thus, using (B 14), the last term on the right-hand side of (B 11) can be expressed as

913 
$$\frac{3}{DeH_{\ell}} \int_{0}^{1} \eta \left[ \int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell} \right] d\eta = -\frac{9}{2H_{\ell}^{2}} \int_{0}^{1} \eta (1-\eta^{2}) \left[ \tilde{A}_{12,0} \right]_{Z_{\ell}=L}^{Z_{\ell}=0} d\eta + \frac{27De}{2H_{\ell}^{4}} \int_{0}^{1} \eta^{2} (1-\eta^{2}) \left[ \tilde{A}_{22,0} \right]_{Z_{\ell}=L}^{Z_{\ell}=0} d\eta + \frac{3L}{H_{\ell}^{3}}.(B \, 15)$$

915 Substituting (B 15) into (B 11) provides the alternative expression for  $\Delta P_{\ell,1}$ ,

916 
$$\Delta P_{\ell,1} = \frac{3}{2De} \int_0^1 (1-\eta^2) \left[ \tilde{A}_{11,0} \right]_{Z_\ell=L}^{Z_\ell=0} d\eta - \frac{9}{2H_\ell^2} \int_0^1 \eta (1-\eta^2) \left[ \tilde{A}_{12,0} \right]_{Z_\ell=L}^{Z_\ell=0} d\eta$$

917 
$$+ \frac{27De}{2H_{\ell}^4} \int_0^1 \eta^2 (1 - \eta^2) \left[ \tilde{A}_{22,0} \right]_{Z_{\ell}=L}^{Z_{\ell}=0} d\eta.$$
(B16)

Under the assumption that L is such that the elastic stresses reach their fully relaxed values by the end of the exit channel, (B 16) shows that the first-order contribution  $\Delta P_{\ell,1}$  is independent of L since the steady-state values of  $\tilde{A}_{11,0}$ ,  $\tilde{A}_{12,0}$ , and  $\tilde{A}_{22,0}$  depend solely on the  $\eta$  coordinate.

# 921 B.2.1. Pressure drop in the exit channel at $O(\tilde{\beta})$ in the low-De limit

To calculate the pressure drop  $\Delta P_{\ell}$  in the exit channel at low Deborah numbers, we use (B 7b)-(B 7c) and (B 10). The elastic normal stress contribution to  $\Delta P_{\ell,1}$  is

924 
$$\Delta P_{\ell,1}^{\rm NS} = \frac{3}{2De} \int_0^1 (1 - \eta^2) \left[ \tilde{A}_{11,0} \right]_{Z_\ell = L}^{Z_\ell = 0} d\eta = -\frac{1296De^3 H''(1)}{35H_\ell^7} \quad \text{for} \quad De \ll 1.$$
(B17)

# E. Boyko, E.J. Hinch and H.A. Stone

925 The elastic shear stress contribution to the pressure drop at  $O(\tilde{\beta})$  is

926 
$$\Delta P_{\ell,1}^{SS} = \frac{3}{DeH_{\ell}} \int_{0}^{1} \eta \left[ \int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell} \right] d\eta, \qquad (B\,18)$$

927 with the integral  $\int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell}$  given as

928 
$$\int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell} \approx \frac{3DeL}{H_{\ell}^{2}} \eta - \frac{81De^{4}H''(1)}{H_{\ell}^{6}} \eta (1-\eta^{2})^{3} \text{ for } De \ll 1, \quad (B\,19)$$

where we have neglected terms multiplying  $e^{-2H_{\ell}L/[3De(1-\eta^2)]} \approx 0$ . Substituting (B 19) into (B 18), we obtain

931 
$$\Delta P_{\ell,1}^{SS} = \frac{3L}{H_{\ell}^3} - \frac{432De^3 H''(1)}{35H_{\ell}^7} \quad \text{for} \quad De \ll 1.$$
(B 20)

Combining the normal and shear stress contributions, (B 17) and (B 20), provides the expression for the pressure drop at  $O(\tilde{\beta})$  in the low-*De* limit

934 
$$\Delta P_{\ell,1} = -\frac{3L}{H_{\ell}^3} + \Delta P_{\ell,1}^{\rm NS} + \Delta P_{\ell,1}^{\rm SS} = -\frac{1728De^3 H''(1)}{35H_{\ell}^7} \quad \text{for} \quad De \ll 1.$$
(B 21)

935 Therefore, the total pressure drop in the exit channel in the low-De limit is

936 
$$\Delta P_{\ell} = \underbrace{(1 - \tilde{\beta})\frac{3L}{H_{\ell}^{3}}}_{\text{Solvent stress}} + \underbrace{-\frac{1296\tilde{\beta}De^{3}H''(1)}{35H_{\ell}^{7}}}_{\text{Elastic normal stress}} + \underbrace{\frac{3L}{H_{\ell}^{3}}\tilde{\beta} - \frac{432\tilde{\beta}De^{3}H''(1)}{35H_{\ell}^{7}}}_{\text{Elastic shear stress}}$$
937 
$$= \frac{3L}{H_{\ell}^{3}} - \frac{1728\tilde{\beta}De^{3}H''(1)}{35H_{\ell}^{7}} \quad \text{for} \quad De \ll 1.$$
(B 22)

Equation (4.3) shows that for a smooth contraction with H'(1) = H'''(1) = 0, the first nonvanishing viscoelastic contribution to the pressure drop in the exit channel at low Deborah numbers is only at  $O(De^3)$  as the O(De) and  $O(De^2)$  contributions are identically zero.

# 941 B.2.2. Pressure drop in the exit channel at $O(\tilde{\beta})$ in the high-De limit

To calculate the pressure drop  $\Delta P_{\ell}$  in the exit channel at high Deborah numbers, we use (B 9b)-(B 9c) and (B 10). The elastic normal stress contribution to  $\Delta P_{\ell,1}$  is

944 
$$\Delta P_{\ell,1}^{\rm NS} = \frac{3}{2De} \int_0^1 (1-\eta^2) \left[ \tilde{A}_{11,0} \right]_{Z_\ell=L}^{Z_\ell=0} \mathrm{d}\eta = \frac{18}{5} De(H_\ell^{-2} - H_\ell^{-4}) \quad \text{for} \quad De \gg 1.$$
(B23)

945 The elastic shear stress contribution to the pressure drop at  $O(\tilde{\beta})$  is

$$\Delta P_{\ell,1}^{\rm SS} = \frac{3}{DeH_{\ell}} \int_0^1 \eta \left[ \int_L^0 \tilde{A}_{12,0} dZ_{\ell} \right] d\eta = \frac{3L}{H_{\ell}^3} + \frac{18}{5} De(H_{\ell}^{-2} - H_{\ell}^{-4}) \quad \text{for} \quad De \gg 1,$$
(B 24)

946

where the integral  $\int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell}$ , after neglecting terms multiplying  $e^{-2H_{\ell}L/[3De(1-\eta^2)]} \approx 0$ , is given as

949 
$$\int_{L}^{0} \tilde{A}_{12,0} dZ_{\ell} \approx \frac{3DeL}{H_{\ell}^{2}} \eta + \frac{9De^{2}(H_{\ell}^{2}-1)}{H_{\ell}^{3}} \eta (1-\eta^{2}) \quad \text{for} \quad De \gg 1.$$
(B 25)

30

Combining the normal and shear stress contributions, (B 23) and (B 24), provides the expression for the pressure drop at  $O(\tilde{\beta})$  in the high-*De* limit,

952 
$$\Delta P_{\ell,1} = -\frac{3L}{H_{\ell}^3} + \Delta P_{\ell,1}^{\rm NS} + \Delta P_{\ell,1}^{\rm SS} = \frac{36}{5} De(H_{\ell}^{-2} - H_{\ell}^{-4}) \quad \text{for} \quad De \gg 1.$$
(B 26)

953 Therefore, the total pressure drop in the exit channel in the high-De limit is

954 
$$\Delta P_{\ell} = (1 - \tilde{\beta}) \frac{3L}{H_{\ell}^{3}} + \underbrace{\frac{18}{5} \tilde{\beta} De(H_{\ell}^{-2} - H_{\ell}^{-4})}_{\underbrace{\ell}} + \underbrace{\frac{3L}{H_{\ell}^{3}} \tilde{\beta} + \frac{18}{5} \tilde{\beta} De(H_{\ell}^{-2} - H_{\ell}^{-4})}_{\underbrace{\ell}}$$

Solvent stress Elastic normal stress

$$= \frac{3L}{H_{\ell}^3} + \frac{36}{5} \tilde{\beta} De(H_{\ell}^{-2} - H_{\ell}^{-4}) \quad \text{for} \quad De \gg 1.$$
 (B 27)

Elastic shear stress

REFERENCES

- ABOUBACAR, M., MATALLAH, H. & WEBSTER, M. F. 2002 Highly elastic solutions for Oldroyd-B and Phan Thien/Tanner fluids with a finite volume/element method: planar contraction flows. J. Non-Newtonian
   *Fluid Mech.* 103 (1), 65–103.
- AGUAYO, J. P., TAMADDON-JAHROMI, H. R. & WEBSTER, M. F. 2008 Excess pressure-drop estimation in contraction and expansion flows for constant shear-viscosity, extension strain-hardening fluids. J. Non-Newtonian Fluid Mech. 153 (2-3), 157–176.
- AHMED, H. & BIANCOFIORE, L. 2021 A new approach for modeling viscoelastic thin film lubrication. J.
   Non-Newtonian Fluid Mech. 292, 104524.
- AHMED, H. & BIANCOFIORE, L. 2023 Modeling polymeric lubricants with non-linear stress constitutive
   relations. J. Non-Newtonian Fluid Mech. 321, 105123.
- ALVES, M. A., OLIVEIRA, P. J. & PINHO, F. T. 2003 Benchmark solutions for the flow of Oldroyd-B and PTT
   fluids in planar contractions. J. Non-Newtonian Fluid Mech. 110 (1), 45–75.
- ALVES, M. A., OLIVEIRA, P. J. & PINHO, F. T. 2021 Numerical methods for viscoelastic fluid flows. *Annu. Rev. Fluid Mech.* 53, 509–541.
- ALVES, M. A. & POOLE, R. J. 2007 Divergent flow in contractions. J. Non-Newtonian Fluid Mech. 144 (2-3),
  140–148.
- BECHERER, P., VAN SAARLOOS, W. & MOROZOV, A. N. 2009 Stress singularities and the formation of
  birefringent strands in stagnation flows of dilute polymer solutions. J. Non-Newtonian Fluid Mech.
  157 (1-2), 126–132.
- BINDING, D. M., PHILLIPS, P. M. & PHILLIPS, T. N. 2006 Contraction/expansion flows: The pressure drop
   and related issues. J. Non-Newtonian Fluid Mech. 137 (1-3), 31–38.
- BIRD, R. B., ARMSTRONG, R. C. & HASSAGER, O. 1987 Dynamics of Polymeric Liquids, volume 1: Fluid
   Mechanics, 2nd edn. John Wiley and Sons.
- BOYKO, E. & STONE, H. A. 2021 Reciprocal theorem for calculating the flow rate–pressure drop relation for
   complex fluids in narrow geometries. *Phys. Rev. Fluids* 6, L081301.
- 981 BOYKO, E. & STONE, H. A. 2022 Pressure-driven flow of the viscoelastic Oldroyd-B fluid in narrow non-
- uniform geometries: analytical results and comparison with simulations. J. Fluid Mech. 936, A23.
   PRAND L. 1047 Vactor and Tangon Analysis, John Wiley and Song
- 983 BRAND, L. 1947 Vector and Tensor Analysis. John Wiley and Sons.
- CHILCOTT, M. D. & RALLISON, J. M. 1988 Creeping flow of dilute polymer solutions past cylinders and spheres. J. Non-Newtonian Fluid Mech. 29, 381–432.
- DANDEKAR, R. & ARDEKANI, A. M. 2021 Nearly touching spheres in a viscoelastic fluid. *Phys. Fluids* 33 (8), 083112.
- DATT, C. & ELFRING, G. J. 2019 A note on higher-order perturbative corrections to squirming speed in
   weakly viscoelastic fluids. J. Non-Newtonian Fluid Mech. 270, 51–55.
- DATT, C., NASOURI, B. & ELFRING, G. J. 2018 Two-sphere swimmers in viscoelastic fluids. *Phys. Rev. Fluids* 3 (12), 123301.
- DATT, C., NATALE, G., HATZIKIRIAKOS, S. G. & ELFRING, G. J. 2017 An active particle in a complex fluid.
   J. Fluid Mech. 823, 675–688.

31

955

- DATTA, S. S., ARDEKANI, A. M., ARRATIA, P. E., BERIS, A. N., BISCHOFBERGER, I., MCKINLEY, G. H.,
  EGGERS, J. G., LÓPEZ-AGUILAR, J. E., FIELDING, S. M., FRISHMAN, A., GRAHAM, M. D., GUASTO,
  J. S., HAWARD, S. J., SHEN, A. Q., HORMOZI, S., MOROZOV, A., POOLE, R. J., SHANKAR, V., SHAQFEH,
  E. S. G., STARK, H., STEINBERG, V., SUBRAMANIAN, G. & STONE, H. A. 2022 Perspectives on
  viscoelastic flow instabilities and elastic turbulence. *Phys. Rev. Fluids* 7, 080701.
- DEBBAUT, B., MARCHAL, J. M. & CROCHET, M. J. 1988 Numerical simulation of highly viscoelastic flows
   through an abrupt contraction. J. Non-Newtonian Fluid Mech. 29, 119–146.
- FERRÁS, L. L., AFONSO, A. M., ALVES, M. A., NÓBREGA, J. M. & PINHO, F. T. 2020 Newtonian and viscoelastic fluid flows through an abrupt 1: 4 expansion with slip boundary conditions. *Phys. Fluids* 32 (4), 043103.
- GAMANIEL, S. S., DINI, D. & BIANCOFIORE, L. 2021 The effect of fluid viscoelasticity in lubricated contacts
   in the presence of cavitation. *Tribol. Int.* 160, 107011.
- GKORMPATSIS, S. D., GRYPARIS, E. A., HOUSIADAS, K. D. & BERIS, A. N. 2020 Steady sphere translation in a viscoelastic fluid with slip on the surface of the sphere. J. Non-Newtonian Fluid Mech. 275, 104217.
- HINCH, E. J., BOYKO, E. & STONE, H. A. 2023 Fast flow of an Oldroyd-B model fluid through a narrow
   slowly-varying contraction. *Submitted*.
- HOUSIADAS, K. D., BINAGIA, J. P. & SHAQFEH, E. S. G. 2021 Squirmers with swirl at low Weissenberg
   number. J. Fluid Mech. 911, A16.
- JAMES, D. F. & ROOS, C. A. M. 2021 Pressure drop of a boger fluid in a converging channel. J. Non-Newtonian
   Fluid Mech. 293, 104557.
- KEILLER, R. A. 1993 Spatial decay of steady perturbations of plane Poiseuille flow for the Oldroyd-B
   equation. J. Non-Newtonian Fluid Mech. 46 (2-3), 129–142.
- 1016 LARSON, R. G. 1988 Constitutive Equations for Polymer Melts and Solutions. Butterworths.
- LI, C., THOMASES, B. & GUY, R. D. 2019 Orientation dependent elastic stress concentration at tips of slender
   objects translating in viscoelastic fluids. *Phys. Rev. Fluids* 4 (3), 031301.
- 1019 MOKHTARI, O., LATCHÉ, J.-C., QUINTARD, M. & DAVIT, Y. 2022 Birefringent strands drive the flow of 1020 viscoelastic fluids past obstacles. J. Fluid Mech. 948, A2.
- 1021 MOORE, M. N. J. & SHELLEY, M. J. 2012 A weak-coupling expansion for viscoelastic fluids applied to 1022 dynamic settling of a body. J. Non-Newtonian Fluid Mech. **183**, 25–36.
- MOROZOV, A. & SPAGNOLIE, S. E. 2015 Introduction to complex fluids. In *Complex Fluids in Biological Systems* (ed. S. E. Spagnolie), pp. 3–52. Springer.
- NIGEN, S. & WALTERS, K. 2002 Viscoelastic contraction flows: comparison of axisymmetric and planar
   configurations. J. Non-Newtonian Fluid Mech. 102 (2), 343–359.
- 1027 OBER, T. J., HAWARD, S. J., PIPE, C. J., SOULAGES, J. & MCKINLEY, G. H. 2013 Microfluidic extensional 1028 rheometry using a hyperbolic contraction geometry. *Rheol. Acta* **52** (6), 529–546.
- 1029 OLDROYD, J. G. 1950 On the formulation of rheological equations of state. *Proc. R. Soc. A* 200 (1063),
   1030 523–541.
- 1031 OWENS, R. G. & PHILLIPS, T. N. 2002 Computational rheology. Imperial College Press.
- 1032 PEARSON, J. R. A. 1985 Mechanics of Polymer Processing. Elsevier.
- REMMELGAS, J., SINGH, P. & LEAL, L G. 1999 Computational studies of nonlinear elastic dumbbell models
   of Boger fluids in a cross-slot flow. J. Non-Newtonian Fluid Mech. 88 (1-2), 31–61.
- RENARDY, M. 2000 Asymptotic structure of the stress field in flow past a cylinder at high Weissenberg
   number. J. Non-Newtonian Fluid Mech. 90 (1), 13–23.
- Ro, J. S. & HOMSY, G. M. 1995 Viscoelastic free surface flows: thin film hydrodynamics of Hele-Shaw and dip coating flows. *J. Non-Newtonian Fluid Mech.* 57 (2-3), 203–225.
- ROTHSTEIN, J. P. & MCKINLEY, G. H. 1999 Extensional flow of a polystyrene Boger fluid through a 4: 1: 4
   axisymmetric contraction/expansion. J. Non-Newtonian Fluid Mech. 86 (1-2), 61–88.
- ROTHSTEIN, J. P. & MCKINLEY, G. H. 2001 The axisymmetric contraction–expansion: the role of extensional rheology on vortex growth dynamics and the enhanced pressure drop. *J. Non-Newtonian Fluid Mech.* 98 (1), 33–63.
- SAPRYKIN, S., KOOPMANS, R. J. & KALLIADASIS, S. 2007 Free-surface thin-film flows over topography:
   influence of inertia and viscoelasticity. J. Fluid Mech. 578, 271–293.
- SAWYER, W. G. & TICHY, J. A. 1998 Non-Newtonian lubrication with the second-order fluid. J. Tribol.
   1047 120 (3), 622–628.
- SOUSA, P. C., COELHO, P. M., OLIVEIRA, M. S. N. & ALVES, M. A. 2009 Three-dimensional flow of Newtonian and Boger fluids in square–square contractions. J. Non-Newtonian Fluid Mech. 160 (2-3), 122–139.

- STEINBERG, V. 2021 Elastic turbulence: an experimental view on inertialess random flow. Annu. Rev. Fluid
   Mech. 53, 27–58.
- 1052 SU, Y., CASTILLO, A., PAK, O. S., ZHU, L. & ZENIT, R. 2022 Viscoelastic levitation. J. Fluid Mech. 943, A23.
- SZABO, P., RALLISON, J. M. & HINCH, E. J. 1997 Start-up of flow of a FENE-fluid through a 4:1:4 constriction in a tube. J. Non-Newtonian Fluid Mech. 72 (1), 73–86.
- TICHY, J. A. 1996 Non-Newtonian lubrication with the convected Maxwell model. *Trans. ASME J. Tribol.* 118, 344–348.
- VAN GORDER, R. A., VAJRAVELU, K. & AKYILDIZ, F. T. 2009 Viscoelastic stresses in the stagnation flow of
   a dilute polymer solution. J. Non-Newtonian Fluid Mech. 161 (1-3), 94–100.
- VARCHANIS, S., TSAMOPOULOS, J., SHEN, A. Q. & HAWARD, S. J. 2022 Reduced and increased flow resistance
   in shear-dominated flows of Oldroyd-B fluids. J. Non-Newtonian Fluid Mech. 300, 104698.
- WESTEIN, E., VAN DER MEER, A. D., KUIJPERS, M. J. E., FRIMAT, J.-P., VAN DEN BERG, A. & HEEMSKERK, J.
   W. M. 2013 Atherosclerotic geometries exacerbate pathological thrombus formation poststenosis in a von Willebrand factor-dependent manner. *Proc. Natl. Acad. Sci. USA* 110 (4), 1357–1362.
- ZHANG, Y. L., MATAR, O. K. & CRASTER, R. V. 2002 Surfactant spreading on a thin weakly viscoelastic
   film. J. Non-Newtonian Fluid Mech. 105 (1), 53–78.
- ZOGRAFOS, K., HARTT, W., HAMERSKY, M., OLIVEIRA, M. S. N., ALVES, M. A. & POOLE, R. J. 2020
   Viscoelastic fluid flow simulations in the e-VROC<sup>TM</sup> geometry. J. Non-Newtonian Fluid Mech. 278, 104222.